



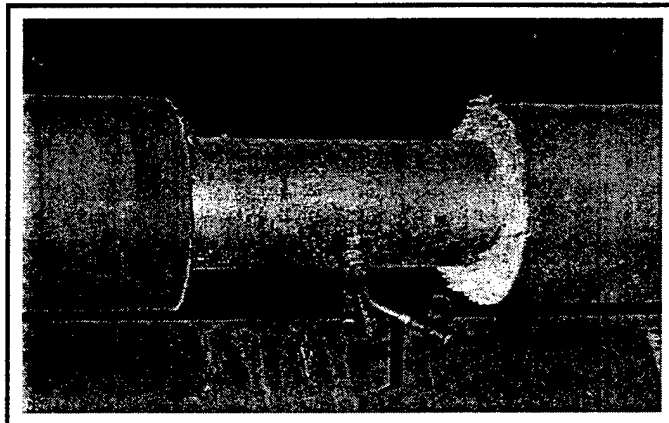
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of Engineers**
Construction Engineering
Research Laboratory

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May 1999

Defense Supply Center Columbus Central Heat Plant Modernization

Plant Assessment

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The Department of Defense (DOD) owns a large number of aging district heating systems, typically consisting of a central heat plant (CHP) and a heat distribution system. Many of these systems are nearing the end of their useful life, and incur significant maintenance and repair costs to keep them operational. This study focused on the CHP at the Defense Supply Center Columbus (DSCC), Columbus, OH to help the installation meet long-term goals of reduced energy consumption and improved air quality. Condition assessment surveys were done at the DSCC CHP. Researchers evaluated the current state of the system, provided a list of modernization options, and proposed a modernization plan.

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Foreword

This study was conducted for the Defense Supply Center Columbus (DSCC), Columbus, OH, under Military Interdepartmental Purchase Request (MIPR) No. SC070060089. The technical monitor was Ed Poprock, DSCC-WIC.

The work was performed by the Energy Branch (CF-E), of the Facilities Division (CF), U.S. Army Construction Engineering Research Laboratory (CERL). The CERL principal investigator was Michael K. Brewer. Mark W. Slaughter is Chief, CECER-CF-E; and Dr. L. Michael Golish is Chief, CECER-CF. The CERL technical editor was William J. Wolfe, Information Technology Laboratory.

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1 Introduction

Background

The Department of Defense (DOD) owns a large number of aging district heating systems, typically consisting of a central heat plant (CHP) and a heat distribution system. Many of these systems are nearing the end of their useful life, and incur significant maintenance and repair costs to keep them operational. Typical system designs were developed when energy costs were low and when energy efficiency was not seen to be as important a factor as it is now. To meet long-term goals of reduced energy consumption and improved air quality, the DOD's energy supply infrastructure must be revitalized. The CHP at Defense Supply Center Columbus (DSCC), Columbus, OH, is one such facility in need of repairs. DSCC tasked the U.S. Army Construction Engineering Research Laboratory (CERL) to help the installation develop a modernization plan to efficiently effect CHP repairs and system improvements.

Objectives

The objectives of this study were to conduct condition assessment surveys of the CHP at the DSCC to determine the existing state of the system, and to provide modernization options to DSCC.

Approach

1. CERL was tasked to conduct site investigations and equipment inspections at DSCC. During site visits from 21-25 October 1996 and 25-27 November 1996, CERL and its contractor, Schmidt Associates Inc. (SAI) conducted operational tests and "cold iron" inspections. Site visits and meetings fiscal year 1997 (FY97) and FY98 have helped to refine the analysis to accommodate potential mission changes.
2. The assessment team reviewed plant machinery history, system schematics, technical manuals, and plant logs (Figures 1 to 10).

3. The team constructed a model of the CHP and HTHW system using HEATMAP and other analysis tools.
4. Historical data, condition assessments, and plant configuration information were analyzed and processed with existing CERL modeling tools.
5. A series of modernization options were outlined, and a modernization plan was proposed to implement the most desirable modernization alternative.

Mode of Technology Transfer

As part of this project, CERL has delivered the HEATMAP model as a turnkey hardware and software package to allow DSCC to manipulate the model parameters for utility planning purposes. CERL has also trained DSCC personnel on the use of HEATMAP.

2 CHP Assessment

During the 21-25 October 1996 site visit, CERL and SAI conducted flue gas analysis at various locations along the flue gas path to evaluate pollution control effectiveness. Inspections were conducted on the furnace grates, forced draft plenums, furnace tubes, generation bank, generator outlet duct, mechanical dust collectors (MDCs), and electrostatic precipitators (ESPs). Appendix A summarizes test data.

During the 25-27 November 1996 site visit, CERL inspected furnace tube failures in Unit #1. At DSCC's request, CERL contracted NALCO* to conduct a tube failure analysis of the tube metal. Appendix B contains the NALCO metallurgical analysis report. NALCO reported that oxygen pitting and long-term overheating of the generator tubes were likely causes of tube failure.

Coal Handling Systems

DSCC reports excessive levels of coal fines in the storage pile runoff. The storage area does have a low curb around it, but does not have any runoff treatment. At an earlier point in time, DSCC had minimized runoff by using coal pile covers. No covers are in use now.

Pneumatic and Electronic Controls

The coal-fired units have a mix of electronic and electro-mechanical controls. The newer gas-fired unit has electronic and mechanical controls installed near the burner front.

DSCC is in the middle of an electrical system upgrade. CERL did not review the upgrade plan or inspect equipment installation.

* NALCO Chemical Co., Naperville, IL 60563-1198.

Combustion Air Flow Systems

The forced draft fan (FDF) takes suction near the roof. The FDF inlet duct forms the outside surface of the generator outlet duct. This is meant to capture a small amount of heat from the flue gas stream. However, the common duct wall between the FDF inlet air duct and generator outlet air duct is corroding due to acid condensation in the outlet ducting. The duct wall has several holes with diameters of 3 to 5 in. due to the flue gas acid corrosion. At the generator outlet, the pressure is about -1.5 in WC. Although the FDF duct pressure in the vicinity of the holes was not measured, it would most likely not be as negative. Therefore, cooler FDF duct air would be drawn into the flue gas stream via the holes and further cool the gas and cause acid condensation on pollution control equipment (Figure 1). Researchers also observed that the Induced Draft (ID) and FD fan motors needed supplemental cooling with large floor fans.

High Temperature Hot Water (HTHW) Generators

Spreader Stoker

The Riley Stokers were inspected by J.W. Chappel from SAI. The rotor blades appear to be set correctly to distribute the coal evenly. However, Chappel recommends feeding coal to the stoker while in a maintenance shutdown to observe the throw of the coal without fire in the furnace. CERL and SAI can provide support in blade setting during shutdown if desired.

Traveling Grate

The grate in Unit #1 was satisfactory for firing in the 1996-1997 heating season. However, some of the components need repair or replacing such as bowed T-bars, bent rails, endclip seals, overgrate seal shoes (which need replacement due to crystallization), and worn skid shoes. The rear right thermocouple is also missing. The bent and worn components may cause the grate to bind as well as leak in tramp air (Figures 2 and 3).

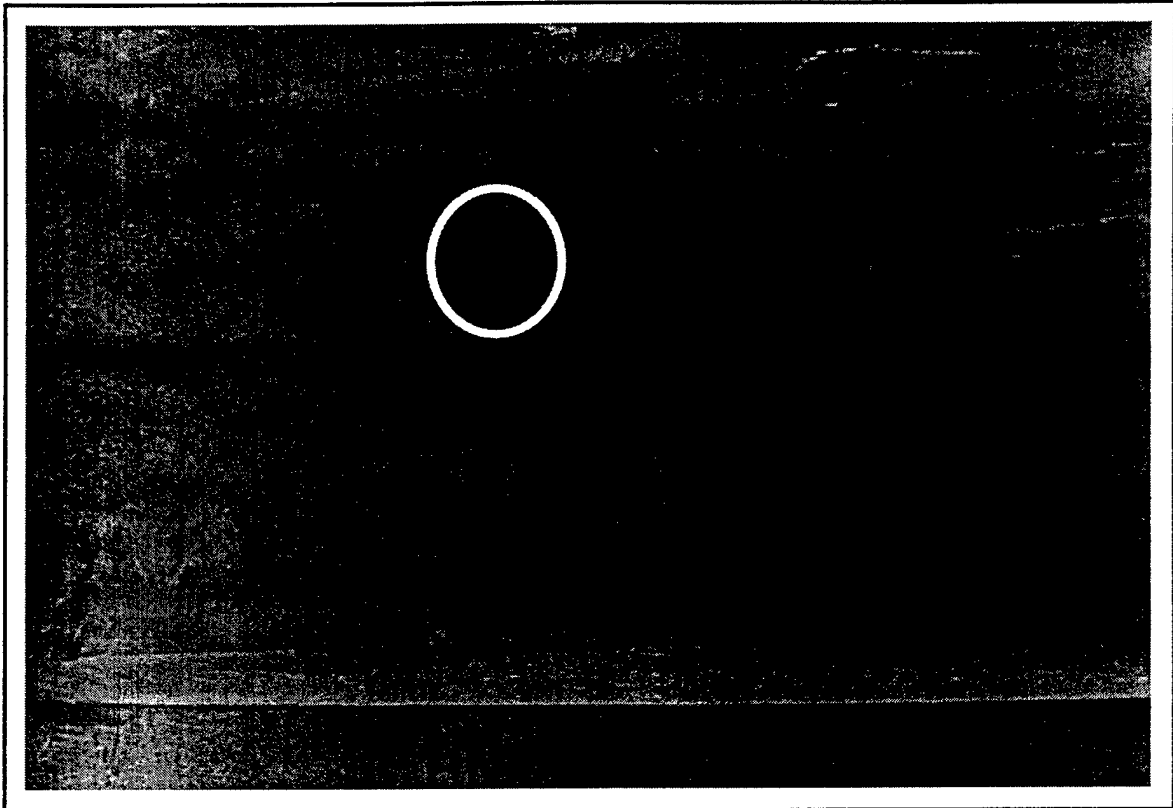


Figure 1. Hole in No. 3 outlet duct.

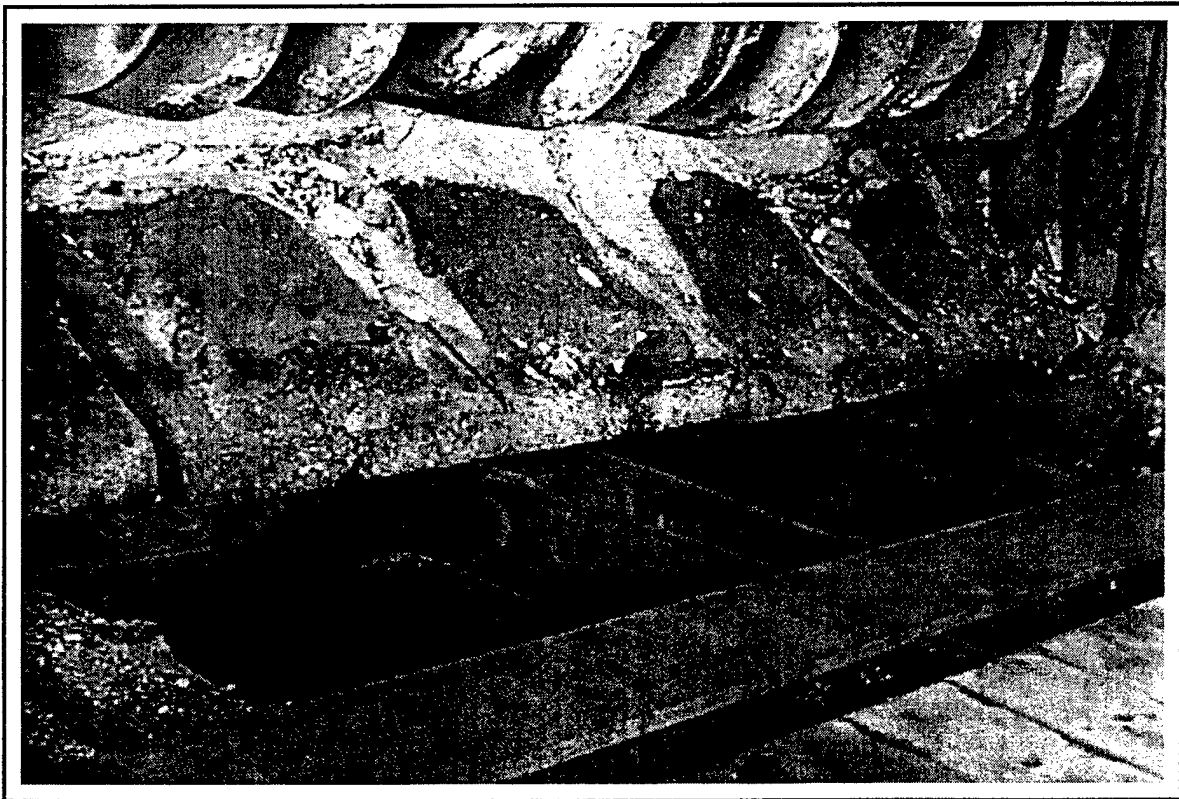


Figure 2. Rear grate seal shoes crystallized.

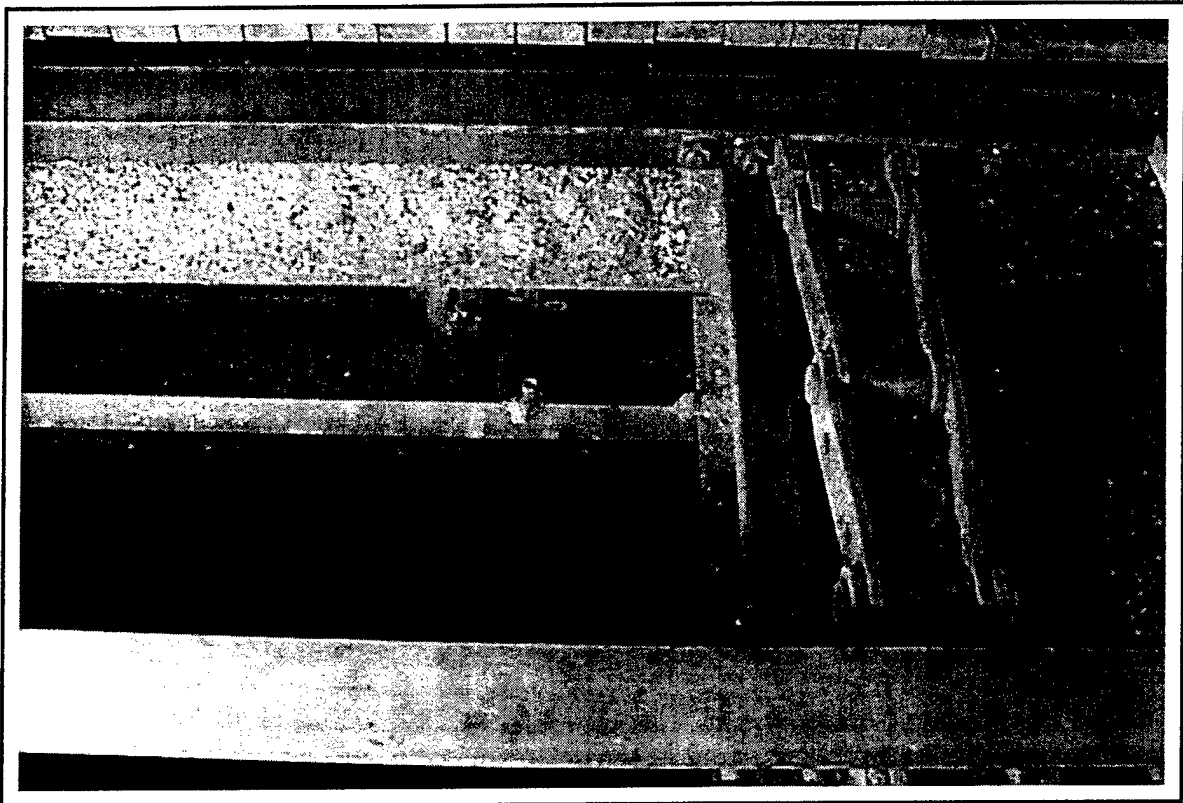


Figure 3. Missing thermocouple, Unit No. 1.

Furnace Tubes

Several tubes in Unit #1 have failed during attempted startup in the 1996-1997 heating season. As noted in the NALCO analysis, widespread oxygen pitting is suspected. The tube sample also showed signs of low level, long-term overheating.

In generator #3, the wall tubes on the right side appear to have been overheated. Some of the tubes have moved away from the wall. Lower portions of some of the wall tubes have metal surface patterns uncharacteristic of normal tubes. The metal irregularities could be due to excessive metal temperatures (Figure 4). At least 25 tubes on the left furnace look newer than the rest of the furnace.

During FY97, DSCC implemented tube repairs to units #1 and #3 to correct the tube failures discovered in FY96.

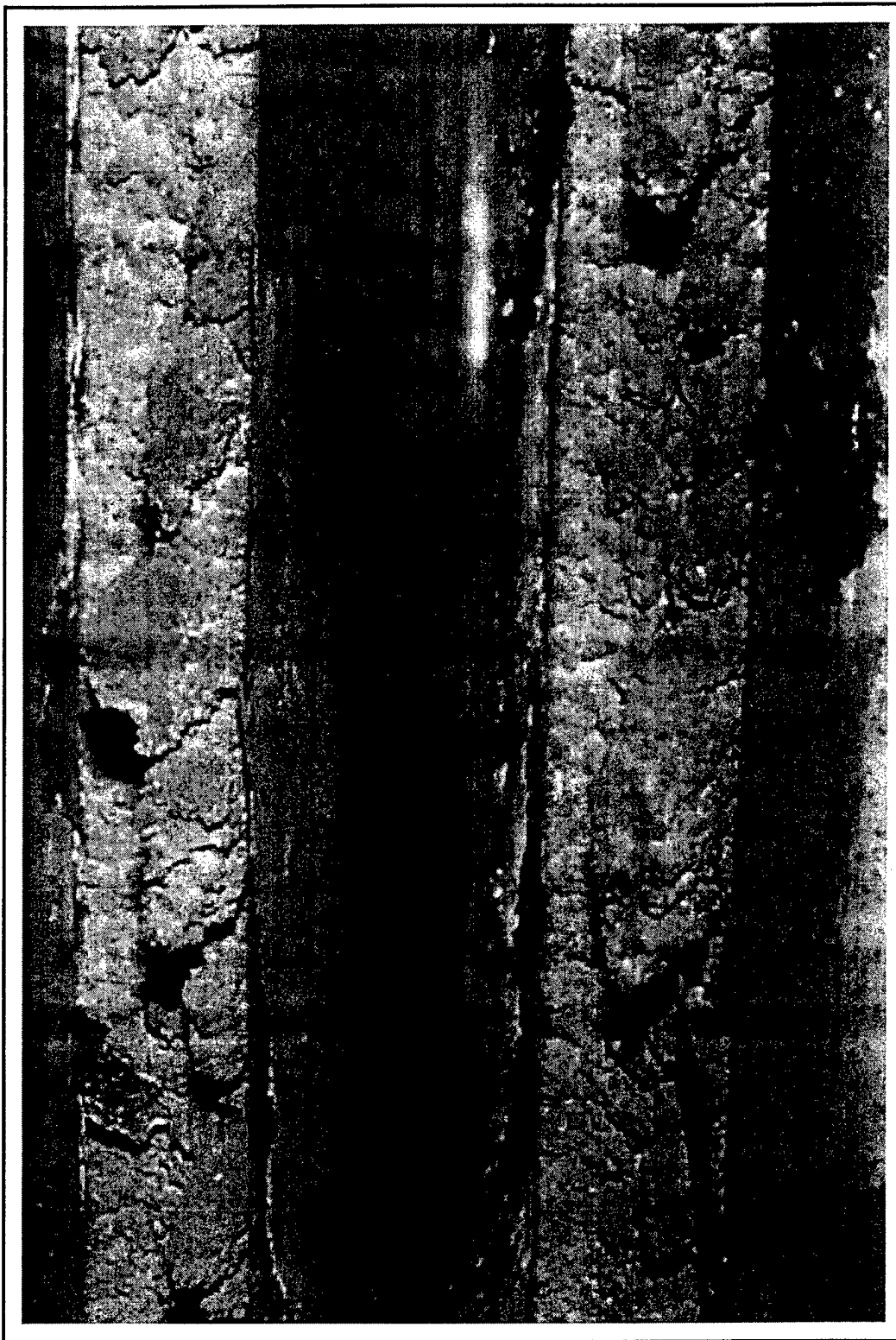


Figure 4. Overhead furnace wall tube, Generator No. 3.

Furnace Casing and Refractory

Large sections of the refractory have become wet from the water leaks in unit #1. It is likely that moisture has migrated into the casing insulation as well (Figure 5). Major portions of the refractory were replaced as part of the retubing in FY97.

Generation Tubes

The tubes were externally inspected from the top and the bottom. The tubes appear to be in good condition.

In the back pass of Unit #3, the refractory has failed in spots. The backwall and part of the side wall tubes are pushed out from the wall. Some of the header plugs are weeping and may need new seals at the next maintenance shutdown. The generation bank tubes also need air lancing to remove debris.

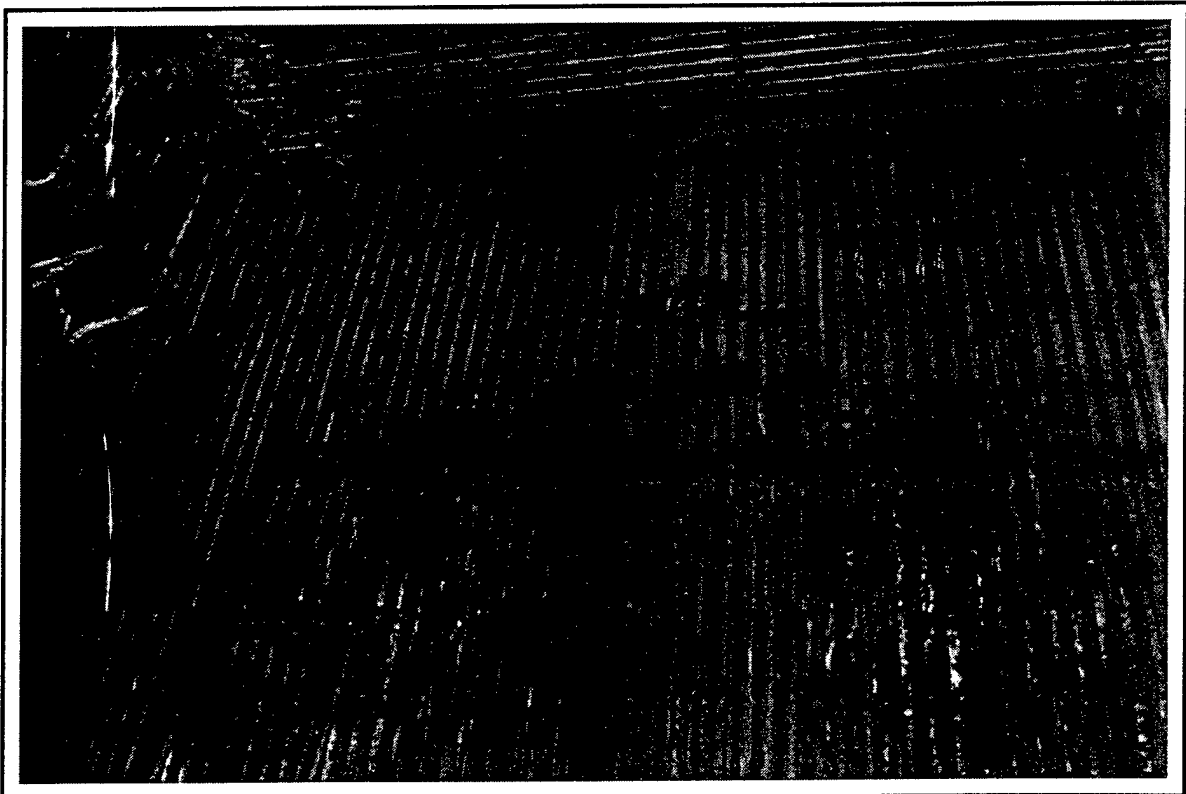


Figure 5. Water soaked refractory, Unit No. 1.

Multi-Cyclone Dust Collectors (MDC)

MDC #1 needs major repairs. Researchers observed a lot of flyash in the east hopper. It was not determined whether the ash was there due to an operational oversight or system malfunction. The bottom portion of the lower tubes is severely worn. The back row of spinners was also clogged with wet ash deposits. The MDC inlet dampers were not working. These dampers allow the operator to remove part of the MDC from service during low loads to keep the flue gas velocity high enough for proper dust collection. Several of the upper tubes were severely worn. The wear was so severe that a hole had developed in Tube E3. Many of the spinners are severely worn as well. At the MDC exit, wet ash has collected on top of the tube sheet. Rope packing is needed in MDC outlet expansion joint to reduce flue gas condensation in that stagnation area.

MDC #3 also requires major repairs. Several of the top tubes and spinners were worn (Figure 6). Dust collector C2 spinner is installed backward. Lower tube C3 is severely cracked and is likely to fall out soon (Figure 7). Maintenance personnel should be aware of the falling object hazard when entering the hopper to inspect or repair the MDC. At least four of the lower tube boots have broken tabs and are falling out of place (Figure 8).

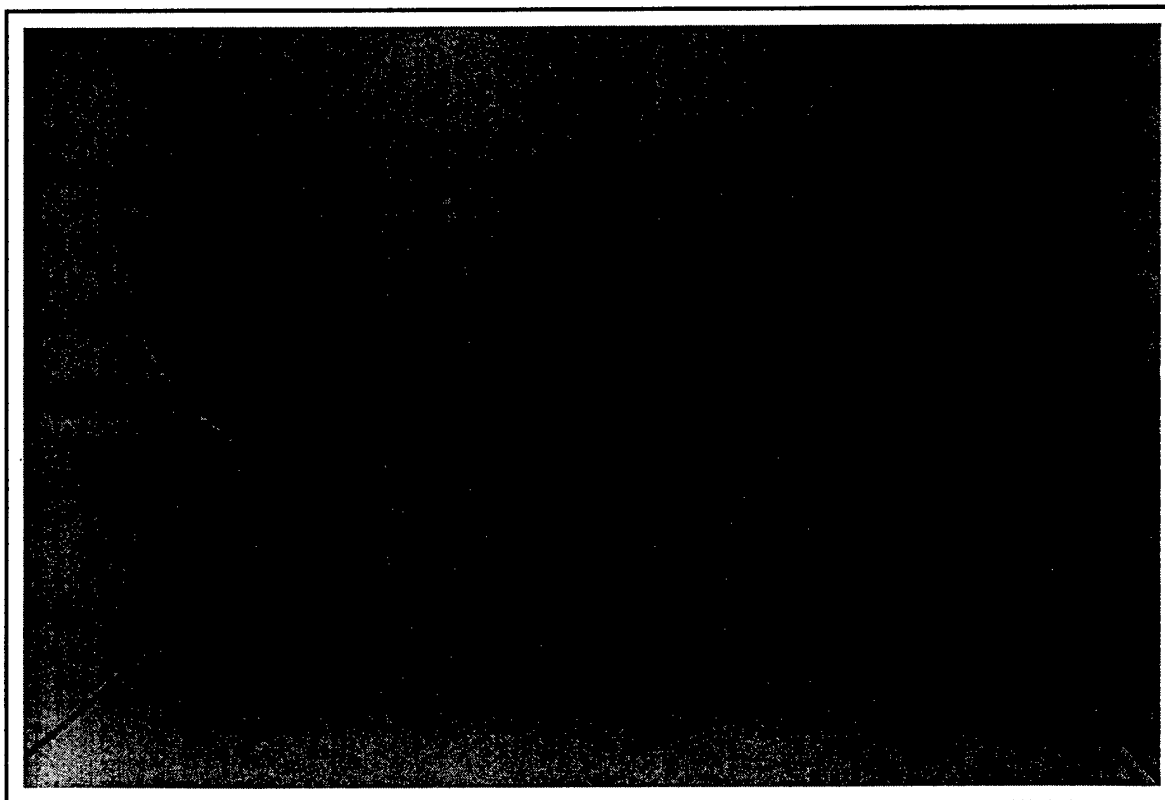


Figure 6. Hole in upper tube, MDC No. 1.

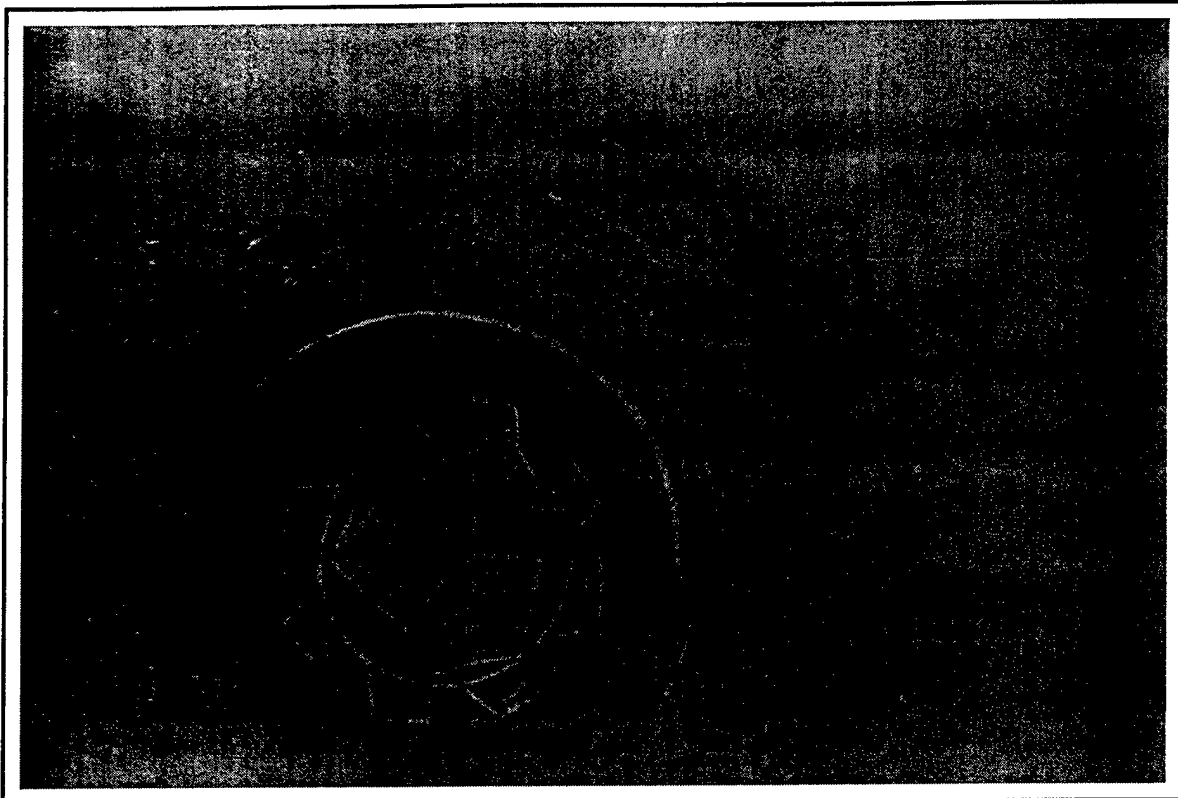


Figure 7. Cracked lower tube, MDC No. 3.



Figure 8. Broken lower tube boot tabs, MDC No. 3.

The MDC is one of the simplest pollution control devices for coal boilers. As the first cleanup device, it removes the greatest amount of particulate. A correctly designed and operated MDC can clean the flue gas of most stoker boilers to compliance standards at steady state condition.

Electrostatic Precipitators (ESP)

The ESPs are in need of major repair or replacement. Moisture is entering the ESP via roof leaks (Figure 9). The plates are bowed and warped. Plate spreader bars have been installed to mitigate the bowing. However, the plates have continued to be overheated, which has been causing further warpage. The overheating may be caused by glowing ash deposits. If the oxygen level in the flue gas is above 9 percent, the carbon in the flyash will continue to burn and generate heat as it is collected on the plates. Oxygen levels of 11 to 12 percent were measured during the November 1996 site visit.

The warping and bowing prevents the wires from being centered between the plates (Figure 10). The ESP must have the wires within 1/2-in. of the mid-point of the gap between the plates. Many of the wires on the ESP are out of position 2 in. or more.

If the ESP plates and wires are in correct alignment and the field controls are properly adjusted, the field voltage should be high enough to cause 50 sparks per minute. If the spark rate is too low, the field will not be strong enough to impart a charge to the dust particles. If it is too high, the electrical discharge will be inefficient and, in the presence of high oxygen, could cause ash fires in the ESP.

Pneumatic Ash Handling System

There were abnormally high levels of ash in some of the ash hoppers. It was not determined whether this was due to an operational oversight or system degradation. The ash silo was being repaired during the October 1996 visit.

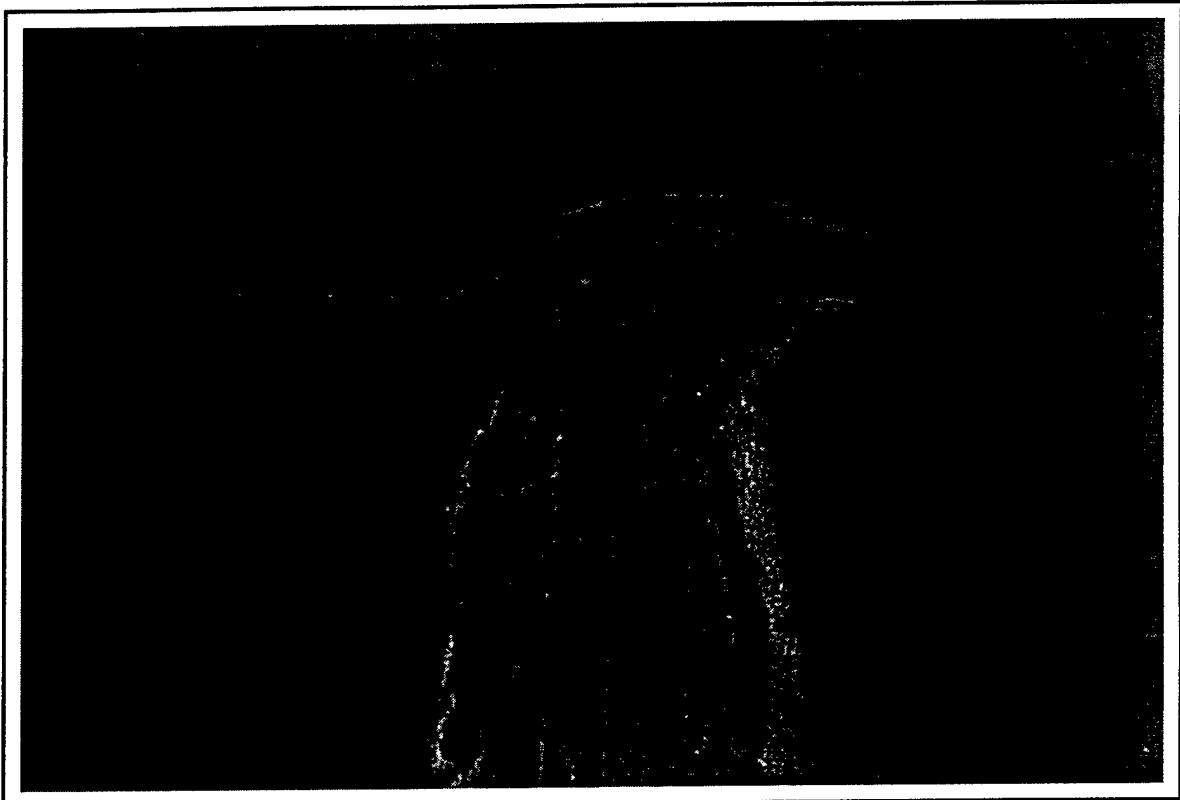


Figure 9. Roof leak in ESP.

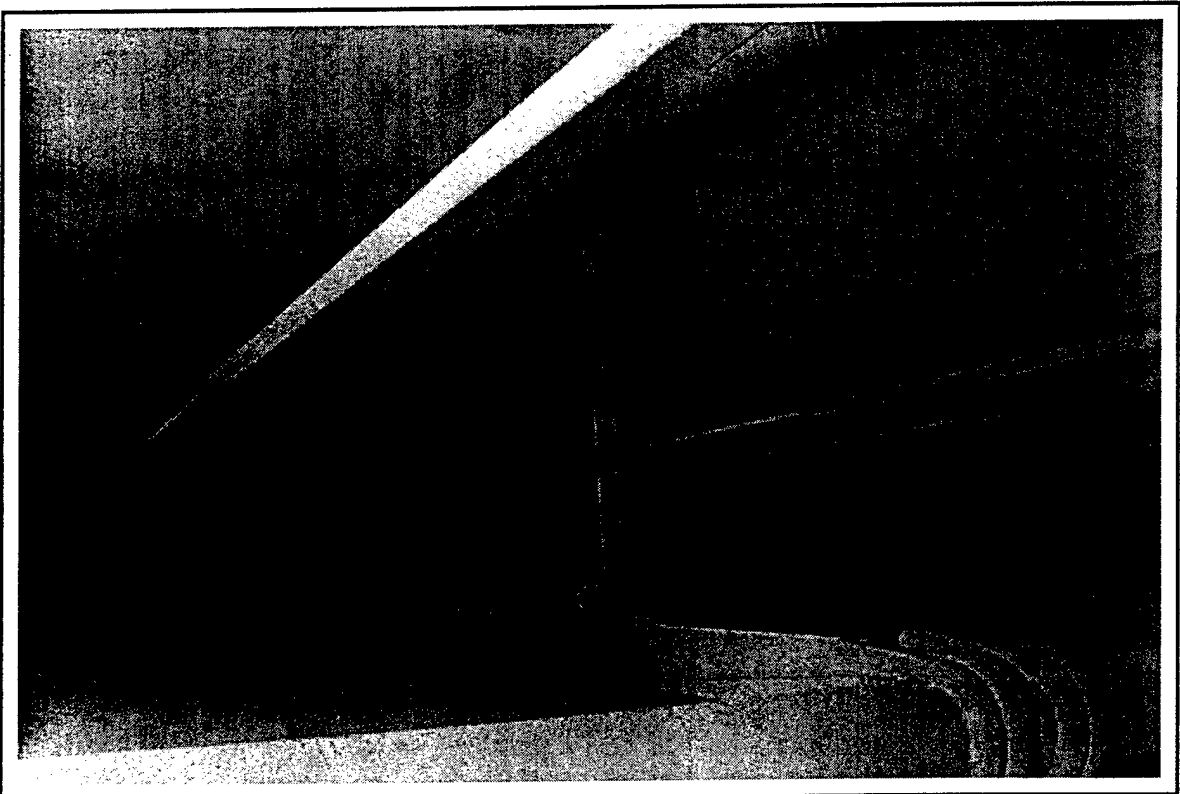


Figure 10. Warped plates and wires off center in ESP.

HTHW Distribution System, Including Piping, Valves, Generator Pumps, and Distribution Pumps

Three of the mechanical rooms were visited. No major problems were noted in the cursory tour. The buildings are mostly served by HTHW to steam converters. A few buildings are served by HTHW to Low Temperature Hot Water (LTHW) converters or HTHW directly. The steam converters are more sensitive to temperature fluctuations. One of the purposes of the small gas-fired unit is to boost the temperature of the HTHW supply during certain conditions so that distant steam converters can produce the required pressure. CERL material engineers conducted a site visit 23 November 1998 to assess the serviceability of the HTHW distribution piping. The external inspection and water samples indicated that the piping is in fair to good condition and is not in danger of imminent failure. Table 1 summarizes inspection and repair status of the entire system.

Table 1. Inspection and repair summary.

Component	Inspected	Condition	Repair
Storage Pile	Nov-96	Coal fines in runoff	
Pneumatic and Electric Controls	NA		Upgrade in progress 96-97
Combustion Air System	Nov-96	Hole in FDF duct; Fan motors overheating	
Spreader Stoker	Nov-96	Static check satisfactory; Recommend coal throw check	
Traveling Grate	Nov-96	Repair and replace worn and bent grate components	
Furnace Tubes	Nov-96	Overheated and pitted tubes	Retubed Units #1 and #3 FY97
Furnace Casing and Refractory	Nov-96	Moisture damage	Replaced during retubing FY97
Generation Tubes	Nov-96	Refractory in backpass of #3 has failed; Leaking header plugs	
Multi-Cyclone Dust Collectors	Nov-96	Broken and worn out tubes; Leaking seals	
Electro-Static Precipitators	Nov-96	Plates bowed and warped; Wires off-center; Leaks; High O ₂ levels	
Pneumatic Ash Handling	Nov-96	High ash levels in hoppers	Repair in progress Nov 96
High Temperature Hot Water Piping and water chemistry	Nov-98	Water samples satisfactory; Water softener may be undersized or ineffective	

Water Treatment Systems

The water chemistry samples drawn by CERL indicated that hardness is being controlled. However, the pH is running too high at 11.5. The hot water system should maintain a pH of 9 to 10.5 to avoid copper corrosion in heat exchangers. The sulfite level should be controlled to 50-100 ppm. Although the samples were less than 50 ppm, some sulfite was lost due to air entrained in the sampling and shipping procedure.

3 CHP and HTHW System Thermal Model

A model was constructed of the CHP and HTHW system using HEATMAP and other analysis tools. Historical data, condition assessments, and plant configuration information will be analyzed and processed with existing CERL modeling tools. CERL delivered the HEATMAP model in October 1998 as a turnkey hardware and software package to allow DSCC to manipulate the model parameters for utility planning purposes. As part of the turnkey package, CERL trained DSCC personnel on the use of HEATMAP. A summary of the HEATMAP output is in Appendix C. A summary of the analysis data sheets are in Appendix D.

Preliminary thermal energy supply analysis has been done on the existing system. Table 2 summarizes the plant model.

Table 2. Distribution Model Summary

Scenario	Annual Fuel (Mbtu/yr)	Peak HTHW Energy (Mbtu/hr)	System Losses (Mbtu/yr)	Piping Construction Cost (\$) **
Log estimates	124,659	78		
101 – HTHW Current Loads	104,280	82.6	10,065	5,775,151
104 – HTHW Load reduced by demolition	60,210	48	3,019	5,595,247
105 – HTHW Load reduced by demolition, dry pipe conversion, and Bldg 41 & 42 small boilers	33,288	25.7	3,302	5,091,478
106 – LTHW Current Load reduced by demolition, dry pipe conversion, and Bldg 41, 42 and 27 small boilers	21,133	18.2	3,619	2,549,957
* Closure not achieved on log reading. Instrumentation has lost calibration. Log estimates adjusted using fuel consumption.				
** Construction costs from HEATMAP default tables. For a new system analysis, the estimating tables would be reviewed and modified to match expected construction practices.				

4 Development and Evaluation of CHP Modernization Options

Plant Alternatives

Over 19 different repair alternatives were calculated over the course of the study. In general, the alternatives were combinations of central plants, decentralized systems, government labor, contracted labor, coal, interruptible gas, firm gas, government O&M, third party O&M, load reductions due to demolition, load reduction due to dry pipe fire protection, baghouse pollution control, and ESP pollution control. All of the data files were provided to DSCC throughout the project. However, to help develop a workable heat utility plan, only the more competitive options are summarized in this report. Additionally, the alternatives are grouped according to the heat loads they serve. DSCC expects to reduce the heating needs due to demolition and conversion to dry pipe fire protection conversion. CERL analyzed the cost of alternatives along a "glide path" from the current building heat load of 79.6 MBTU/hr to 37.5 MBTU/hr. Appendix D includes a data summary of repair alternatives for the CHP.

Basis for Life Cycle Costing for DSCC Project

Information/estimates were furnished by SAI and CERL. The most current version of the WinLCCID software was used for the calculations. A life cycle of 25 years was used with residual values for the central plant improvements as central plants have life expectancies of twice that of small commercial grade equipment. Appendix E shows the LCCID output.

OM&R costs for central plants were derived from industrial plants in Ohio, U.S. Army coal plant data, and DSCC cost data. Government manpower costs were derived from the most current wage grade pay scale for Columbus, OH. Central plant energy costs were estimated from 4-year averages of Redbook fuel data and HEATMAP analysis. SAI furnished new construction costs. Third party OM&R costs were scaled to that seen at Ohio industrial stoker plants.

Energy rate information were provided by Bonnie Stillwagon, DESC (tel. [703] 767-8544). DESC is currently providing firm and interruptible gas to other Federal Government customers in the area (DOE). Based on the cost of interruptible natural gas to DOE from September 1996 to February 1997, and on an estimate of the cost from the city gate to the burner tip, the cost would be \$4.66/Mbtu. A price survey done in June 98 determined that Columbia Gas would charge \$1.50 per mcf (MBtu) to deliver gas to DSCC. Assuming the June 1998 city gate cost of \$2.80/mcf, the delivered cost to DSCC would be about \$4.30/mcf for interruptible gas. The utility, Columbia Gas (POC Patti Spangler, tel. [614] 460-2157), would charge a firm rate of about \$6.00/Mbtu. The cost for DESC-provided #2 fuel oil would be \$0.63/gal (\$4.53/Mbtu).

The mix of fuel usage was determined assuming that the plant would operate from October to April. For gas use, firing for most of the 6 months would be on interruptible gas with firing on #2 backup only for the few days (zero to 10 days) of a curtailment.

Decentralized boiler OM&R was estimated from decentralized studies and market surveys conducted for Fort Meade and Fort Drum. Since the boilers will be gas only, firm gas will need to be purchased. For decentralized furnaces, 286,650 Btu/hr hot air furnaces will heat the buildings. Three FTE's will remain to operate and maintain the decentralized furnaces. OM&R estimated at about \$100/year/unit.

Full Load Alternatives

Table 3 tabulates the top six options for the current load. This set of options assumes that all the current buildings heated in 1997 will continue to need heating and that the government would operate the systems. Some of the buildings will continue to have wet pipe fire protection even though the material stored in them does not require heating. The peak building load is approximately 79 MBTU/hr.

The base case is to convert the coal stokers to gas and provide oil backup. Although coal is the status quo, significant capital must be invested in the pollution control system. Decentralized boilers have the least life cycle cost due to the large savings in labor and maintenance. However, the large capital investment has a long payback. The Army recommends energy conservation projects have savings to investment ratios (SIR's) above 3. Decentralization will save some energy by avoiding the line losses but the fuel bill will be higher due to the premium paid for firm gas.

Table 3. Full load (Scenario 101) heating options.

Name	Capital Cost	Labor Cost	OM&R	Fuel	LCC NPV	SIR	DPP
Gas Conversion - Oil BU	1,500,000	594,168	169,813	450,046	18,450,230		
Coal - Baghouse	2,570,000	594,168	319,596	210,725	17,381,820	2.1	12
Coal - ESP	2,760,000	594,168	319,596	210,725	17,530,620	1.8	14
New Gas Unit - Oil BU	3,270,000	594,168	169,813	450,046	19,835,840	0.1	99
Decentralized - Boilers	4,764,176	130,663	100,100	520,443	15,441,100	2	9
Decentralized - Furnaces	8,957,231	130,663	27,100	492,239	17,782,330	1.1	21

Reduced Load Alternatives (Demolition)

Table 4 tabulates the top 3 options for a reduced load. The coal-fired options were dropped as they will be even less competitive with a reduced load. Even though the fuel cost may drop for the coal options, the labor, and operations and maintenance costs will not drop proportionately to the fuel usage decline. For the central plant, only one coal HTHW unit would be converted to gas. The full staff is left in the plant even though the work load would be significantly reduced by not burning coal. The peak building heating load will be approximately 60 MBTU/hr.

Two factors increase the competitiveness of the decentralized options. First, the demolition reduces the construction cost about 25 percent. Second, the annual costs of the decentralized options are dramatically less than those of the central plant option. At this load point, with a SIR of 4, using decentralized boilers is a viable alternative.

Table 4. Reduced load (Scenario 104) heating options.

Option	Name	Capital Cost	Labor Cost	OM&R	Fuel	LCC NPV	SIR	DPP
3.40	Gas Conversion - Oil BU	1,895,000	594,168	184,899	325,846	17,135,530		
8.40	Decentralized - Boilers	3,640,000	87,369	76,937	380,284	11,358,890	4.7	4
9.40	Decentralized - Furnaces	6,051,209	87,369	30,986	364,919	12,661,800	2.2	8

Reduced Load Alternatives (Demolition, Dry Pipe Conversion)

Table 5 tabulates the top 3 options for a reduced load. For the central plant, only one coal HTHW unit would be converted to gas. The full staff is left in the plant even though the work load would be significantly reduced by not burning coal. The load is reduced even more as almost 1 million sq ft of building space are allowed to go cold once the fire protection system is converted to a dry pipe system. Some consideration must be given to heating the lavatory areas with small heating systems. The cost of converting the fire protection is included in the option capital cost.

These options also include the cost of installing small boilers at Buildings 41 and 42. For this set of options, the fixed costs associated with the central plant make it uneconomical when compared to decentralized plants. There is not enough load and load density to make the central plant viable. CERL also analyzed a set of scenarios that included the cost of a small boiler in Building 27. However, those calculations show that decentralized systems are still the best alternative with a greatly reduced heating load.

Table 5. Reduced load (Scenario 105) heating options.

Option	Name	Capital Cost	Labor Cost	OM&R	Fuel	LCC NPV	SIR	SIR
3.50	Gas Conversion - Oil BU	3,030,584	594,168	184,899	208,051	17,395,280	0.0	0.0
8.50	Decentralized - Boilers	3,495,584	87,369	48,643	233,521	10,752,480	19.3	1
9.50	Decentralized - Furnaces	4,694,067	87,369	23,186	226,197	11,242,330	5.7	3

Analysis Summary

With the present building load, it is desirable to select the option with the lowest first cost as the other alternatives do not have a satisfactory payback. CERL and Schmidt cost estimates show that converting to gas in at least one of the coal fired units is less costly than installing a baghouse or new ESP. Not repairing or replacing the ESP is not a prudent course of action if the central plant is to be maintained.

If the long-term plan is to demolish excess space and install dry pipe fire protection, decentralized heating is the most life cycle cost effective. The savings in labor and fuel will rapidly payback the capital cost differential. The difference in cost between decentralized boilers and furnaces is not large. An assessment of each building's comfort needs should be done to determine which system best serves the occupants. The total costs for the decentralized boiler

option was slightly lower as the existing HTHW/Steam converter mechanical rooms were assumed to be satisfactory locations for the package boilers. Much of the building steam heat system was assumed to be serviceable for the new boilers. Individual gas furnaces will require more gas piping in the building. However, point-of-use gas furnaces and gas radiant heaters may best serve the building heating needs. The effect of the change in load on alternative costs is shown in Figures 11-13.

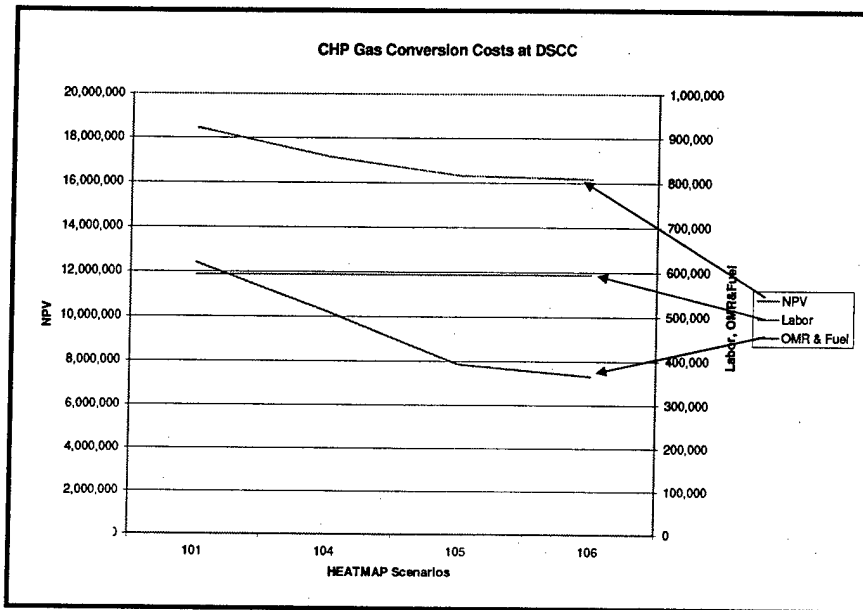


Figure 11. Gas conversion costs with decreasing load.

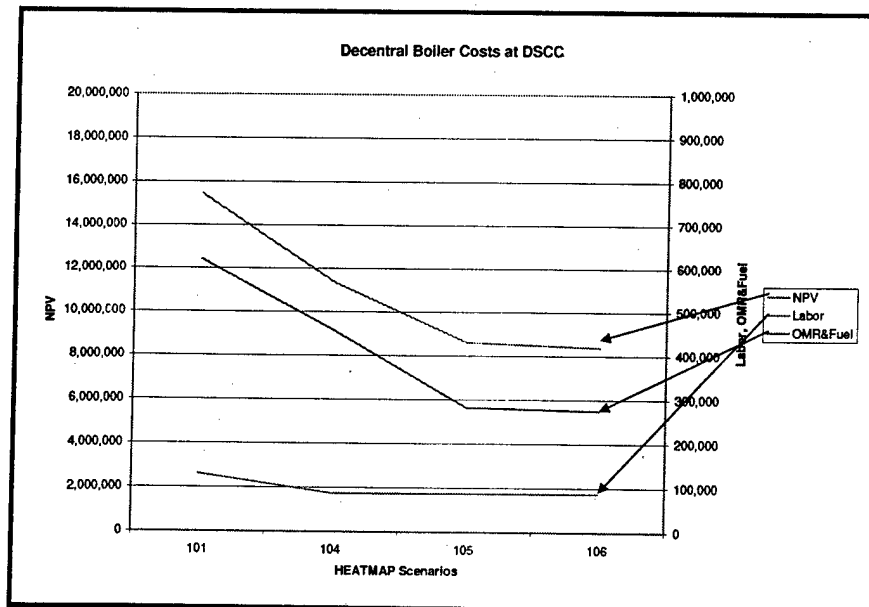


Figure 12. Decentralized boiler costs with decreasing load.

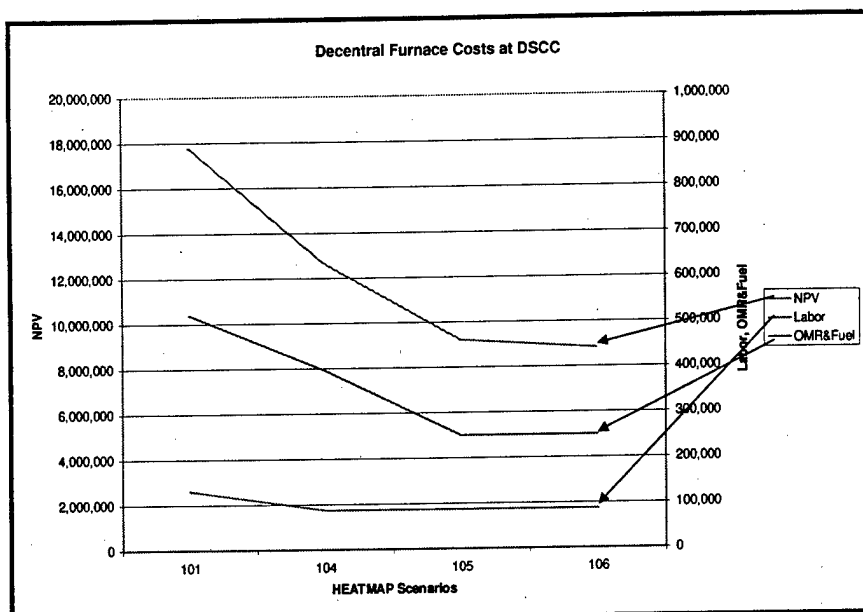


Figure 13. Decentralized furnace costs with decreasing load.

These figures indicate that, if the expected load reduction occurs, decentralized heating will be the most economical heating strategy. However, converting all of the existing buildings to decentralized heating is not currently cost effective.

5 Plant Modernization Plan

Based on the results of the study, CERL and its contractor, Schmidt and Associates, recommend a heat utility modernization schedule be developed. The team recommends short- and long-term actions to modernize the heating systems.

Short Term

Until a demolition schedule is agreed upon, the central plant will need to be maintained. The current pollution control system is need of repair. Plant records have shown that one coal boiler and the smaller gas boiler have carried the load though a whole winter. If a gas curtailment occurs, two coal boilers will be needed to meet a peak load of 80 MBTU/hr. If some buildings were allowed to have minimal heating, one boiler might be able to meet the load. DSCC's planners need to determine a reasonable schedule for funding of the demolition of the excess buildings and conversion of the remaining building to decentralized heating. It is likely that the central plant will need to operate at least two to five more heating seasons. If continued operation of coal is desired, repairs to the MDC should be conducted this summer as a minimum to reduce the cost risks associated with emission compliance. SAI has estimated that the cost to replace the MDC *alone* is about \$80K in the context of a larger repair project. The cost of doing that one repair may be much higher as the mobilization costs will not be spread over as many work items. If a conversion of one boiler to gas with oil backup can be effected quickly, that will greatly reduce the emission compliance risk while waiting for the demolition and dry pipe conversion to occur.

Long Term

The long range goal should be to decentralize if the demolition and dry pipe conversion will occur. If the current load will be maintained, then the coal-fired units should be converted to gas with oil backup.

Plan Development

CERL and its contractor, SAI, can provide detailed information on implementing the most desirable modernization alternative once it is clear what load must be served. To develop construction specifications the Louisville District Corps of Engineers Office can be consulted. They can provide a variety of design, contracting, and construction services to implement the heating system modernization.

The CERL technical point of contact for this project is Michael Brewer, (217) 352-6511, X-7375 (voice), (217) 373-3430 (fax). The mailing address is:

Commander and Director
U.S. Army Construction Engineering Research Laboratory
ATTN: CF-E/M. Brewer
PO Box 9005
Champaign, IL 61826-9005

6 Conclusion

1. This study conducted condition assessment surveys of the CHP at the DSCC to determine the existing state of the system.
2. The results of the surveys were analyzed, and alternative modernization options were derived from this information.
3. A modernization plan was proposed to implement the most desirable alternative, and to train DSCC personnel in the use of the proposed hardware and software.

Appendix A: Site Visit Data Sheets

Utility Modernization Analysis	Site General Data		
<div style="border: 1px solid black; padding: 10px; margin: 10px 0;"><p>Notice to users: This spreadsheet is to assist a base or command engineer assess the economic viability of several energy supply options. It contains data extracted from site visits, HEATMAP analysis, EIS files, LCCID program files and historical cost data. For more information about the analysis contact the Utilities Division, USACERL, Champaign, IL 61826-9005 (800)872-2375 ext 5505.</p></div>			
<table style="width: 100%;"><tr><td style="width: 40%;">Input Section</td><td style="width: 60%; text-align: center;"><u>Fill in all shaded boxes</u></td></tr></table>		Input Section	<u>Fill in all shaded boxes</u>
Input Section	<u>Fill in all shaded boxes</u>		
<div style="margin-bottom: 10px;">Installation Name: <input style="width: 90%;" type="text" value="Defense Supply Center Columbus, OH"/></div> <div style="margin-bottom: 10px;">Installation POCs <input style="width: 90%;" type="text" value="Ed Poprock"/></div> <div style="margin-bottom: 10px;">MACOM POC <input style="width: 90%;" type="text"/></div> <div style="margin-bottom: 10px;">Project Title <input style="width: 90%;" type="text" value="Plant Modernization at DSCC"/></div> <div style="margin-bottom: 10px;">Project Description <div style="border: 1px solid black; height: 60px; width: 100%;"></div></div> <div style="display: flex; justify-content: space-between; margin-bottom: 10px;"><div>Estimated Cost <input style="width: 80%;" type="text"/></div><div>Form #/Work Order <input style="width: 80%;" type="text"/></div></div> <div style="display: flex; justify-content: space-between; margin-bottom: 10px;"><div>Design Status (0-100%) <input style="width: 80%;" type="text"/></div><div>Status of 1391 (0-100%) <input style="width: 80%;" type="text"/></div></div> <div style="margin-bottom: 10px;">Designer <input style="width: 90%;" type="text"/></div> <div style="margin-bottom: 10px;">Design POC <input style="width: 90%;" type="text"/></div> <div style="display: flex; justify-content: space-between; margin-bottom: 10px;"><div>Design Completion Date <input style="width: 80%;" type="text"/></div><div>Projected Project Start Date <input style="width: 80%;" type="text"/></div></div> <div style="border: 1px solid black; padding: 10px; margin-top: 20px;"><p>Note to user: Calculated fields are in blue text. Data input fields are in black or red text. Check the field comments and links before overriding a calculated field.</p></div>			

Utility Modernization Analysis

Site General Data

Site Information

Utility Rate Information:

Natural Gas Utility Rates:

Cooling Rate \$/thermfrom through Firm Boiler Rate \$/thermfrom through

Elect/Gas Use Cost Ratio:

Electric Utility Rates:

Summer Demand \$/kWfrom through Ratchet %from through Winter Demand \$/kWEnergy \$/kWh

Energy Ratio

Smr. EI/Gas: Wntr EI/Gas: Demand/Gas

Fuel rate Information:

#2 Oil (\$/gal) \$/MBTU Coal Spec: #6 Oil (\$/gal) \$/MBTU Coal (\$/ton) \$/MBTU Gas (\$/ccf) \$/MBTU

Int

Gas (\$/ccf) \$/MBTU

Firm

Annual Degree Days:

Heating Cooling

NOTE: Review demand charge calculations to determine appropriate values to enter for number of applicable months.

NOTE: The above rates should include any applicable taxes and surcharges.

Chillers

	Chiller #	Chiller #	Chiller #	Chiller #	
Capacity	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	tons (circle one)
Type	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	(cent., recip., screw, absorb)
Manufacturer	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	
Age	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	
Last Inspection Date	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	
Condition	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	
Primary Fuel	<input type="text"/>	<input type="text"/>	<input type="text"/>	<input type="text"/>	

Distribution System Length feetDiameter of Main inchesType of Distribution System: Direct Buried, Above Ground, or Shallow Trench (circle one)Distribution System is: Loop, Branched, or Combination (circle one)

Utility Modernization Analysis		Site General Data	
Technology Considerations			
Is it replacement in kind?	YES/NO <input type="text" value="y"/>		
Different Technology Considerations:	YES/NO	Fuels Considered:	Primary Alternate
Central Energy Plants	<input type="text" value="Y"/>	Natural Gas	<input type="text" value="Y"/>
Decentralized system	<input type="text" value="Y"/>	Fuel Oil	<input type="text" value="Y"/>
Standalone Satellite Plants and Distribution	<input type="text" value="Y"/>	Coal	<input type="text" value="Y"/>
Satellite Plants with Common Distribution	<input type="text"/>	Wood	<input type="text"/>
Other	<input type="text"/>	Other	<input type="text"/>
Describe Other <input style="width: 400px;" type="text"/>			
Heating		Cooling	
LTHW	<input type="text" value="In Bldg"/>	Electric	<input type="text"/>
HTHW	<input type="text" value="CHP"/>	Engine Driven Chillers	<input type="text"/>
Steam	<input type="text" value="In Bldg"/>	Absorption	<input type="text"/>
Distribution System Type:	YES/NO	Distribution System Type:	YES/NO
Above Ground	<input type="text" value="Y"/>	Above Ground	<input type="text"/>
Shallow Trench	<input type="text" value="N"/>	Shallow Trench	<input type="text"/>
Direct Buried	<input type="text"/>	Direct Buried	<input type="text"/>
Master Planning Coordination:			
Are the projects compatible with CURRENT infrastructure projects?		<input type="text"/>	
Are the projects compatible with PLANNED infrastructure projects?		<input type="text"/>	
Condition Ratings:			
Is the Installation Status Report (ISR) used to rate the central plants?		<input type="text"/>	
Is the Installation Status Report used to rate the distribution systems?		<input type="text"/>	
Is anything being done to reevaluate ISR readings?		<input type="text"/>	
Plant Personnel:		Telephone/Fax	
Plant Engineer	Ed Poprock	(614) 692-6703, FAX 3093	
Plant Foreman	<input type="text"/>	(614) 692-2717, 3645	
Plant Operator	<input type="text"/>	<input type="text"/>	
Plant Maintenance	<input type="text"/>	<input type="text"/>	
Heating/Cooling Mechanical Shop:		Telephone/Fax	
Chief	<input type="text"/>	<input type="text"/>	
Foreman	Art Thompson	<input type="text"/>	
Maintenance	<input type="text"/>	<input type="text"/>	
Utility Bills		<input type="text"/>	
Gas Co Rep	Patti Spangle Columbia Gas	(614) 460-2157	

Utility Modernization Analysis				Heat Plant Data	
Existing Equipment					
Plant Data					
Plant Peak Load		lbs/hr or MBbu/hr (circle one)			
Plant No-Load Load		lbs/hr or MBbu/hr (circle one)			
Reported M/U Rate (Daily Ave)		gallons			
Plant Annual Coal Use	4617	Tons	13500	Btu/lbs	124659 MBTU/yr
Plant Annual Steam Prod.		KLbs stm	180	Days Oper.	0.0% Ave Eff
Peak Plant Capacity	180	lbs/hr or MBTU/hr (circle one)			
Plant Annual Oil Use		Gallons	139,000	Btu/gal	0 MBTU/yr
Plant Annual Gas Use		ccf	0.1	MBTU/ccf	0 MBTU/yr
Boilers					
	Unit #1	Unit #2	Unit #3		
Capacity	70	40	70	lbs/hr or MBTU/hr (circle one)	
Type	WT	WT	WT	(water tube, fire tube)	
Convection Heating Surface	6993		6993	ft2	
Water Wall Surface	1238	582	1238	ft2	
Total HS	8231	2441	8231		
MAWP Pressure	500	500	500		
Oper Pressure					
Safety Set Press					
Manufacturer	IBW	Geo. Marker	Erie City		
Built	1962	1995	1962		
NBPV# No.	M2913	FCW-11-941	M2911		
Last Inspection Date					
Condition					
Grate	Riley				
Burner Data					
Primary Fuel	Coal	N. Gas	Coal		
Alternate Fuel	none	none	none		
Controls					
Safety Viv					
WS Internal		Sl. Scale			
FS Internal		No Hot Spt			

Utility Modernization Analysis

Plant Water Treatment Data

Water Treatment System

Water Treatment Equipment
and Chemicals used
or Contractor (please list)

Makeup Rate gallons/day lbs/hr (ave) gpm
Ave Annualized Makeup Rate Peak No/Low Load

Water Treatment Beds

Regeneration Manual/Auto
Bed Types Zeolite Softner/H-OH IX
Number of Beds
Bed Diameter (in) X-Area (ft2) Max rate gpm
Vessel Ht. (in) Bed Ht. (est) Bed Vol (est) ft3
Resin Cap (18-24K/ft3)

Water Analysis

Hardness ppm
Conductivity microMho
TDS ppm

Utility Modernization Analysis

Boiler Data Sheet

Boiler Test Data (Unit #3) - DSCC, Columbus, OH

Enerac ESP Inlet		25-Nov-96					
Time		16:20	16:30	16:40	16:50	17:00	17:10
Combustion Eff(%)		84.4	84.3	84.2	84.9	85	85.6
Amb Temp (F)		65	66	65	65	65	67
Stack Temp (F)		254	262	265	283	265	251
O2 (dry)		12.0%	11.8%	11.9%	10.4%	11.1%	11.1%
CO(ppm)		26	25	23	29	16	14
CO2		7.7%	7.9%	7.9%	9.1%	8.5%	8.5%
Combustibles		0.11%	0.11%	0.11%	0.11%	0.11%	0.11%
Boiler outlet (in WC)							
Excess Air %		108.0%	104.0%	105.0%	80.0%	91.0%	92.0%
NO (pm)		189.0	182.0	182.0	237.0	210.0	171.0
NO2 (ppm)		0	0	0	0	4	0
NOx (ppm)		189	182	182	237	213	171
SOx (ppm)		385	399	399	461	433	409

Plant/Gage Readings

Flue Gas Temp (F)	371	371	373	369	369	364
Oxygen %	7.6	7.5	7.6	8.3	7.6	6.7
H2OFlow(Klbs/hr)	490.3	502.3	503.7	505.4	505.6	505.8
Btu Out(KBtu/hr)	26800	28500	28600	33900	34800	35600
H2O Temp In (F)	367	364	364	343	342	340
H2O Temp Out (F)	426	427	427	423	426	426
Furn Press (in WC)	-0.12	-0.08	-0.08	-0.08	-0.06	-0.07
Last Pass (in WC)	-1.1	-1.1	-1.1	-1.5	-1.5	-1.5
ID Fan Inlet (in WC)	-1.6	-1.6	-1.7	-2.6	-2.6	-2.5
Opacity	1.6	1.4	19.8	2.5	2.6	1.6
HW Inlet (psig)	328	330	333	335	335	334
HW Outlet (psig)	346	345	346	349	350	350

Generator Outlet Data

Oxygen %	8.1	8.1	8.3	9.6	8.3	7.6
Combustibles %	0	0.1	0	0	0	0.2
CO(ppm)	20	21	22	23	27	0
Temperature (F)	391	394	396	397	408	394
Static Press(in H2O)	-0.65	-0.7	-0.71	-0.86	-1.4	-1.0

Mechanical Collector Input

Oxygen %	8.5	8.1	8.4	6.3	8.8	7.6
CO(ppm)	0	0.1	0	0.1	0.1	0.2
Combustibles %	32	32	26	58	22	0
Temperature (F)	374	374	375	371	376	369
Static Press(in H2O)	-0.64	-0.71	-0.7	-0.86	-1.4	-1.0

Mechanical Collector Output

Oxygen %	8.6	8.8	7.8	8.3	8.5	7.9
CO(ppm)	0.1	0.1	0.1	0.1	0.1	0.2
Combustibles %	30	30	24	31	0	0
Temperature (F)	368	369	370	365	368	364
Static Press(in H2O)	-1.4	-1.55	-1.5	-2.7	-2.6	-2.15

Utility Modernization Analysis

Boiler Calc. Sheet I

Boiler Test Data

ESP Outlet

Ave. Enerac Data

25-Nov-96

(ESP Inlet)

Time	16:45
Combustion Eff(%)	84.7
Amb Temp (F)	66
Stack Temp (F)	263
O2 (dry)	11.4%
CO(ppm)	22
CO2	8.3%
Combust	0.11%
Boiler outlet (in WC)	
Excess Air %	96.7%
NOx (pm)	195
NOx (pm)	1
NOx (pm)	196
SOx (ppm)	414

Fuel (Btu/lb) 13500

Calculated

Excess Air	63.90%
Eff w/o rad	84.99%
Rad Loss	1.50%
Eff w/rad	83.5%

Fuel Curve

Btu/lb	12048
Excess Air	65.0%
Eff w/o rad	83.5%
Rad Loss	1.5%
Eff w/rad	82.0%

Ave. Plant/Gage Readings

Flue Gas Temp (F)	370
Oxygen %	7.6
H2OFlow(Klbs/hr)	502.2
Btu Out(KBtu/hr)	31367
H2O Temp In (F)	353
H2O Temp Out (F)	426
Furn Press (in WC)	-0.08
Last Pass (in WC)	-1.3
ID Fan Inlet (in WC)	-2.1
Opacity	4.92
HW Inlet (psig)	333
HW Outlet (psig)	348

Ave. Generator Outlet Data

Oxygen %	8.3
Combustibles %	0.1
CO(ppm)	19
Temperature (F)	397
Static Press(in H2O)	-0.89

Ave. Mechanical Collector Input

Oxygen %	8.0
CO(ppm)	0.08
Combustibles %	28
Temperature (F)	373
Static Press(in H2O)	-0.89

Ave. Mechanical Collector Output

Oxygen %	8.3
CO(ppm)	0.12
Combustibles %	19
Temperature (F)	367
Static Press(in H2O)	-1.98

Utility Modernization Analysis					Boiler Calc. Sheet II			
Coal Boilers				Flue Gas Losses				
HHV	Btu/lb 13500	T amb (F) 396.7	Flue gas (F) 80	Dry Gas 0.09531	Water Vapor 0.03977	Unacctd. 0.01500	Total Loss 15.01%	
Combustion Eff	84.99%			Stoichiometric Excess Air		Dry gas loss includes sensible heat in water vapor. Water vapor loss include fuel moisture and H2 formation. 1.5% unaccounted in coal.		
Fuel	% lb/lb AF	lb/lbmol	lbmol/lb AF	lbmol/lb AF	lbmole/lb AF			
C	70.41%	12	0.05868	Balance C, H2 and S for stocimetric conditions. Balance O2, N2 at excess air conditions.				
H2	4.83%	2	0.02415					
O2	8.28%	32	0.00259					
N2	1.41%	28	0.00050					
S	1.01%	32	0.00032					
H2O (liq)	8.05%	18	0.00447	Solution balances the combustion equation for stoichiometric conditions and then calculates excess air and recalculates flue gas products and properties				
Ash	6.08%	MW	Mole Fract					
Total	100.07%							
Air				0.32037002				
N2	79.00%			0.25319359				
O2	21.00%			0.06730463				
Incremental Excess Air				0.04301				
Excess Air %				64%				
Flue Gas				% Gas Vol (dr Dry Gas Fract LbMoles/lb fuel)				
O2	8.33%	8.33%	0.08333	Assume 2% carbon loss to ash (98% C forms CO2)				
CO (ppm)	18.83	0.00%	0.00002					
CO2	not meas							0.05750
Combustibles	0.05%	0.05%	0.00050					
NOx (ppm)		0.00%	0.00000					
SOx (ppm)		0.00%	0.00000					
H2O				0.02862				
N2				0.25357				
SO2				0.00032				
				0.42386				
				346.7				
				447.981481				
Gas	Polynomial Coeff		deg F deg K	cp	cp ave (Btu/lb lbmole/lb fuel)	Btu/lb fuel	deg F	
CO2	a	b	c	10.5933175	10.5933175	0.05750	0.60913164	
SO2	10.34	0.00274	-195500	10.2408724	10.2408724	0.00032	0.00323228	
H2O	7.7	0.0053	0.00000083	8.55611835	8.55611835	0.02862	0.24489512	
N2	8.22	0.00015	0.00000134	6.94798148	6.94798148	0.41528328	2.88538056	
O2	6.5	0.001	-187700	7.45029383	7.45029383	0.04301	0.32043064	
Sum						4.06307024		
Polynomial equations from Perry's Chemical Handbook Table 3-181, Originally from US Bureau of Mines Bull 371, 1934 and USBM Bull 477, 1948.								

Utility Modernization Analysis

Boiler Data Sheet

Boiler Test Data (Unit #3) - DSCC, Columbus, OH

Enerac ESP Inlet

25-Nov-96

Time	16:00	16:10	16:11	16:13	16:15
Combustion Eff(%)			86.1%	82.2%	79.9%
Amb Temp (F)			66	66	66
Stack Temp (F)			124	204	232
O2 (dry)			15.6%	12.6%	12.9%
CO(ppm)			10	18	28
CO2			3.0%	4.7%	4.6%
Combustibles			0.00%	0.04%	0.11%
Boiler outlet (in WC)					
Excess Air %			259%	135%	141.0%
NO (pm)			79	143	172
NO2 (ppm)			0	1	0
NOx (ppm)			79	143	172
SOx (ppm)			46	267	351

Plant/Gage Readings

Flue Gas Temp (F)	366	369			
Oxygen %	9.3	6.9			
H2OFlow(Klbs/hr)	484.8	489.3			
Btu Out(KBtu/hr)	25100	26700			
H2O Temp In (F)	368	367			
H2O Temp Out (F)	422	426			
Furn Press (in WC)	-0.03	-0.09			
Last Pass (in WC)	-1.1	-1.0			
ID Fan Inlet (in WC)	-1.4	-1.4			
Opacity	1.2	1.4			
HW Inlet (psig)	326	328			
HW Outlet (psig)	341	346			

Generator Outlet Data

Oxygen %	8.6	8.3			
CO(ppm)	0	0			
Combustibles %	24	17			
Temperature (F)	384	388			
Static Press(in H2O)	-0.63	-0.57			

Mechanical Collector Input

Oxygen %	8.5	8.3			
CO(ppm)	0	0			
Combustibles %	29	25			
Temperature (F)	370	370			
Static Press(in H2O)	-0.55	-0.57			

Mechanical Collector Output

Oxygen %	8.8	8.7			
CO(ppm)	0	0.1			
Combustibles %	27	30			
Temperature (F)	365	366			
Static Press(in H2O)	-1.3	-1.2			

Utility Modernization Analysis

Boiler Calc. Sheet I

Boiler Test Data

Fuel (Btu/lb) 13500

Ave. Enerac Data

25-Nov-96

Calculated

(ESP Inlet)

Time	16:09
Combustion Eff(%)	82.7%
Amb Temp (F)	66
Stack Temp (F)	187
O2 (dry)	13.7%
CO(ppm)	19
CO2	4.1%
Combust	0.05%
Boiler outlet (in WC)	
Excess Air %	178.3%
NOx (pm)	131
NOx (pm)	0
NOx (pm)	131
SOx (ppm)	221

Excess Air	65.40%
Eff w/o rad	85.25%
Rad Loss	1.50%
Eff w/rad	83.8%
Fuel Curve	
MBtu/gal	13500
Excess Air	65.0%
Eff (w/o rad)	83.6%
Rad Loss	1.5%
Eff (w/rad)	82.1%

Ave. Plant/Gage Readings

Flue Gas Temp (F)	368
Oxygen %	8.1
H2O Flow(Klbs/hr)	487.1
Btu Out(KBtu/hr)	25900
H2O Temp In (F)	368
H2O Temp Out (F)	424
Furn Press (in WC)	-0.06
Last Pass (in WC)	-1.05
ID Fan Inlet (in WC)	-1.4
Opacity	1.3
HW Inlet (psig)	327
HW Outlet (psig)	344

Ave. Generator Outlet Data

Oxygen %	8.5
CO(ppm)	0.0
Combustibles %	21
Temperature (F)	386
Static Press(in H2O)	-0.60

Ave. Mechanical Collector Input

Oxygen %	8.4
CO(ppm)	0.00
Combustibles %	27
Temperature (F)	370
Static Press(in H2O)	-0.56

Ave. Mechanical Collector Output

Oxygen %	8.8
CO(ppm)	0.05
Combustibles %	29
Temperature (F)	366
Static Press(in H2O)	-1.25

Utility Modernization Analysis					Boiler Calc. Sheet II		
Coal Boilers				Flue Gas Losses			
HHV	Btu/lb 13500	T amb (F) 386.0	Flue gas (F) 80	Dry Gas 0.09272	Water Vapor 0.03977	Unacctd. 0.01500	Total Loss 14.75%
Combustion Eff	85.25%		Stoichiometric Excess Air				
Fuel	% lb/lb AF	lb/lbmol	lbmol/lb AF	lbmol/lb AF	lbmole/lb AF	Dry gas loss includes sensible heat in water vapor. Water vapor loss include fuel moisture and H2 formation. 1.5% unaccounted in coal.	
C	70.41%	12	0.05868	Balance C, H2 and S for stoichiometric conditions. Balance O2, N2 at excess air conditions.			
H2	4.83%	2	0.02415				
O2	8.28%	32	0.00259				
N2	1.41%	28	0.00050				
S	1.01%	32	0.00032				
H2O (liq)	8.05%	18	0.00447				
Ash	6.08%	MW	Mole Fract	Solution balances the combustion equation for stoichiometric conditions and then calculates excess air and recalculates flue gas products and properties			
Total	100.07%						
Air				0.32037002			
N2	79.00%				0.25319359		
O2	21.00%				0.06730463		
Incremental Excess Air				0.04402			
Excess Air %				65%			
Flue Gas	% Gas Vol (dr Dry Gas Fract LbMoles/lb fuel)						
O2	8.45%	8.45%	0.08450				
CO (ppm)	20.50	0.00%	0.00002				
CO2	not meas			0.05750	Assume 2% carbon loss to ash (98% C forms CO2)		
Combustibles	0.00%	0.00%	0.00000				
NOx (ppm)		0.00%	0.00000				
SOx (ppm)		0.00%	0.00000				
H2O				0.02862			
N2				0.25357			
SO2				0.00032			
				0.42453			
			deg F 336.0				
			deg K 442.055556				
Gas	Polynomial Coeff		deg F	deg K	cp	cp ave (Btu/lb lbmole/lb fuel)	Btu/lb fuel deg F
CO2	a	b	c	-195500	10.5507876	10.5507876	0.05750 0.60668611
SO2	7.7	0.0053	0.00000083	10.2050873	10.2050873	0.00032	0.00322098
H2O	8.22	0.00015	0.00000134	8.54816191	8.54816191	0.02862	0.24466739
N2	6.5	0.001		6.94205556	6.94205556	0.41907063	2.90921159
O2	8.27	0.000258	-187700	7.42352114	7.42352114	0.04402	0.32675668
Polynomial equations from Perry's Chemical Handbook Table 3-181, Originally from US Bureau of Mines Bull 371, 1934 and USBM Bull 477, 1948.						Sum	4.09054276

Utility Modernization Analysis

Boiler Data Sheet

Boiler Test Data (Unit #3) - DSCC, Columbus, OH

Enerac ESP Inlet

26-Nov-96

Time	8:40	8:50	9:00	9:10	9:20	9:30
Combustion Eff(%)	83.4	83.4	82.1	82.7	82.6	82.6
Amb Temp (F)	47	46	46	45	45	45
Stack Temp (F)	267	272	275	277	278	281
O2 (dry)	11.7%	11.4%	12.2%	11.7%	11.8%	11.7%
CO(ppm)	25	25	25	27	31	28
CO2	8.0%	8.2%	7.6%	8.0%	7.9%	8.0%
Combustibles	0.11%	0.11%	0.11%	0.11%	0.11%	0.10%
Boiler outlet (in WC)						
Excess Air %	121.0%	115.0%	133.0%	121.0%	123.0%	121.0%
NO (pm)	209.0	221.0	224.0	239.0	225.0	229.0
NO2 (ppm)	8	9	13	15	15	15
NOx (ppm)	216	230	237	254	239	243
SOx (ppm)	426	447	408	427	416	421

Plant/Gage Readings

Flue Gas Temp (F)	340	346	342	344	348	347
Oxygen %	7.1	8	6.9	7	7.7	7.3
H2O Flow(Klbs/hr)	510	510.7	511.6	512.3	510.7	513.6
Btu Out(KBtu/hr)	35100	35500	35000	35300	35400	35600
H2O Temp In (F)	326	330	323	322	326	327
H2O Temp Out (F)	422	422	420	421	422	422
Furn Press (in WC)	-0.09	-0.09	-0.07	-0.06	-0.1	-0.08
Last Pass (in WC)	-1.3	-1.6	-1.8	-1.8	-1.8	-1.7
ID Fan Inlet (in WC)	-2.9	-2.2	-2.3	-2.3	-2.4	-3.2
Opacity	25	30	34	34	31	28
HW Inlet (psig)	299	301	298	296	303	301
HW Outlet (psig)	312	319	315	312	320	318

Generator Outlet Data

Oxygen %	7.8	8.5	8.4	8.5	8.4	8.6
Combustibles %	0.1	0.1	0.1	0.1	0.1	0.1
CO(ppm)	20	26	31	21	24	28
Temperature (F)	343	347	343	341	345	344
Static Press(in H2O)	-1.3	-1.4	-1.4	-1.45	-1.5	-1.45

Mechanical Collector Input

Oxygen %	7.7	8.7	8.4	8.7	8.6	8.4
CO(ppm)	0.1	0.1	0.1	0.1	0.1	0.1
Combustibles %	32	31	35	35	30	32
Temperature (F)	363	367	363	365	367	368
Static Press(in H2O)	-1.3	-1.4	-1.4	-1.5	-1.5	-1.45

Mechanical Collector Output

Oxygen %	8.5	8.9	8.7	8.7	8.7	9
CO(ppm)	0.1	0.1	0.1	0.1	0.1	0.1
Combustibles %	30	31	30	35	29	34
Temperature (F)	350	353	351	349	351	351
Static Press(in H2O)	-2.7	-3.0	-3.0	-3.5	-3.1	-3.1

Utility Modernization Analysis

Boiler Calc. Sheet I

Boiler Test Data

Fuel (Btu/lb) 13500

Ave. Enerac Data
(ESP Inlet)

26-Nov-96

Time	9:05
Amb Temp (F)	82.8
Amb Temp (F)	46
Stack Temp (F)	275
O2 (dry)	11.8%
CO(ppm)	27
CO2	8.0%
Combust	0.11%
Boiler outlet (in WC)	
Excess Air %	122.3%
NOx (pm)	225
NOx (pm)	13
NOx (pm)	237
SOx (ppm)	424

Calculated

Excess Air	64.33%
Eff w/o rad	86.63%
Rad Loss	1.50%
Eff w/rad	85.1%

Fuel Curve

MBtu/gal	12048
Excess Air	64.0%
Eff (w/o rad)	85.2%
Rad Loss	1.3%
Eff (w/rad)	83.9%

Ave. Plant/Gage Readings

Flue Gas Temp (F)	345
Oxygen %	7.3
H2O Flow (Klbs/hr)	511.5
Btu Out (KBtu/hr)	35317
H2O Temp In (F)	326
H2O Temp Out (F)	422
Furn Press (in WC)	-0.08
Last Pass (in WC)	-1.7
ID Fan Inlet (in WC)	-2.6
Opacity	30.33
HW Inlet (psig)	300
HW Outlet (psig)	316

Ave. Generator Outlet Data

Oxygen %	8.4
Combustibles %	0.1
CO(ppm)	25
Temperature (F)	344
Static Press (in H2O)	-1.42

Ave. Mechanical Collector Input

Oxygen %	8.4
CO(ppm)	0.1
Combustibles %	33
Temperature (F)	366
Static Press (in H2O)	-1.43

Ave. Mechanical Collector Output

Oxygen %	8.8
CO(ppm)	0.1
Combustibles %	32
Temperature (F)	351
Static Press (in H2O)	-3.1

Utility Modernization Analysis						Boiler Calc. Sheet II	
Coal Boilers				Flue Gas Losses			
HHV	Btu/lb	T amb (F)	Flue gas (F)	Dry Gas	Water Vapor	Unacctd.	Total Loss
Combustion Eff	13500	343.8	80	0.07896	0.03977	0.01500	13.37%
Fuel	% lb/lb AF	lb/lbmol	lbmol/lb AF	Stoichiometric	Excess Air	Dry gas loss includes sensible heat in water vapor. Water vapor loss include fuel moisture and H2 formation. 1.5% unaccounted in coal.	
C	70.41%	12	0.05868	Balance C, H2 and S for stocimetric conditions. Balance O2, N2 at excess air conditions.			
H2	4.83%	2	0.02415				
O2	8.28%	32	0.00259				
N2	1.41%	28	0.00050				
S	1.01%	32	0.00032				
H2O (liq)	8.05%	18	0.00447				
Ash	6.08%	MW	Mole Fract	Solution balances the combustion equation for stoichiometric conditions and then calculates excess air and recalculates flue gas products and properties			
Total	100.07%						
Air							
N2	79.00%			0.32037002			
O2	21.00%			0.25319359			
Incremental Excess Air				0.06730463	0.04330		
Excess Air %					64%		
Flue Gas		% Gas Vol (dr Dry Gas Fract	LbMoles/lb fuel				
O2	8.37%	8.37%	0.08367				
CO (ppm)	25.00	0.00%	0.00003				
CO2	not meas			0.05750	Assume 2% carbon loss to ash (98% C forms CO2)		
Combustibles	0.10%	0.10%	0.00100				
NOx (ppm)		0.00%	0.00000				
SOx (ppm)		0.00%	0.00000				
H2O				0.02862			
N2				0.25357			
SO2				0.00032			
				0.42470			
		deg F	293.8				
		deg K	418.62963				
Gas	Polynomial Coeff	a	b	c	cp	cp ave (Btu/lb) lbmole/lb fuel	Btu/lb fuel deg F
CO2		10.34	0.00274	-195500	10.3715009	10.3715009	0.05750 0.59637686
SO2		7.7	0.0053	0.00000083	10.0641952	10.0641952	0.00032 0.00317651
H2O		8.22	0.00015	0.00000134	8.51763047	8.51763047	0.02862 0.24379351
N2		6.5	0.001		6.91862963	6.91862963	0.41635825 2.88062852
O2		8.27	0.000258	-187700	7.30696976	7.30696976	0.04330 0.31635543
						Sum	4.04033082
Polynomial equations from Perry's Chemical Handbook Table 3-181, Originally from US Bureau of Mines Bull 371, 1934 and USBM Bull 477, 1948.							

Utility Modernization Analysis

Boiler Data Sheet

Boiler Test Data (Unit #3) - DSCC, Columbus, OH

Enerac ESP Inlet

26-Nov-96

Time	8:00	8:10	8:20	8:30	9:40	
Combustion Eff(%)	84.6	84.0	84.2	83.8		
Amb Temp (F)	51	50	48	48		
Stack Temp (F)	263	272	273	273		
O2 (dry)	10.9%	11.0%	10.8%	11.1%		
CO(ppm)	27	25	28	29		
CO2	8.7%	8.6%	8.8%	8.5%		
Combustibles	0.11%	0.11%	0.11%	0.11%		
Boiler outlet (in WC)						
Excess Air %	104%	106%	101%	108%		
NO (pm)	218	201	204	209		
NO2 (ppm)	5	0	4	4		
NOx (ppm)	223	201	207	212		
SOx (ppm)	438	493	482	492		

Plant/Gage Readings

Flue Gas Temp (F)					345	
Oxygen %					7.4	
H2OFlow(Klbs/hr)					510.8	
Btu Out(KBtu/hr)					35200	
H2O Temp In (F)					324	
H2O Temp Out (F)					421	
Furn Press (in WC)					-0.09	
Last Pass (in WC)					-1.7	
ID Fan Inlet (in WC)					-3.3	
Opacity					30	
HW Inlet (psig)					299	
HW Outlet (psig)					315	

Generator Outlet Data

Oxygen %					8.4	
Combustibles %					0.1	
CO(ppm)					30	
Temperature (F)					345	
Static Press(in H2O)					-1.45	

Mechanical Collector Input

Oxygen %					8.6	
CO(ppm)					0.1	
Combustibles %					36	
Temperature (F)					369	
Static Press(in H2O)					-1.45	

Mechanical Collector Output

Oxygen %					9.1	
CO(ppm)					0.1	
Combustibles %					35	
Temperature (F)					352	
Static Press(in H2O)					-3.2	

Utility Modernization Analysis

Boiler Calc. Sheet I

Boiler Test Data

Fuel (Btu/lb) 13500

Ave. Enerac Data
(ESP Inlet)

26-Nov-96

Calculated

Time	8:32
Combustion Eff(%)	84.2
Amb Temp (F)	49
Stack Temp (F)	270
O2 (dry)	11.0%
CO(ppm)	27
CO2	8.7%
Combust	0.11%
Boiler outlet (in WC)	
Excess Air %	104.8%
NOx (pm)	208
NOx (pm)	3
NOx (pm)	211
SOx (ppm)	476

Excess Air	64.75%
Eff w/o rad	86.57%
Rad Loss	1.50%
Eff w/rad	85.1%

Fuel Curve

MBtu/gal	13500
Excess Air	64.0%
Eff (w/o rad)	85.2%
Rad Loss	1.3%
Eff (w/rad)	83.9%

Ave. Plant/Gage Readings

Flue Gas Temp (F)	345
Oxygen %	7.4
H2OFlow(Klbs/hr)	510.8
Btu Out(KBtu/hr)	35200
H2O Temp In (F)	324
H2O Temp Out (F)	421
Furn Press (in WC)	-0.09
Last Pass (in WC)	-1.7
ID Fan Inlet (in WC)	-3.3
Opacity	30.00
HW Inlet (psig)	299
HW Outlet (psig)	315

Ave. Generator Outlet Data

Oxygen %	8.4
Combustibles %	0.10
CO(ppm)	30
Temperature (F)	345
Static Press(in H2O)	-1.45

Ave Mechanical Collector Input

Oxygen %	8.6
CO(ppm)	0.10
Combustibles %	36
Temperature (F)	369
Static Press(in H2O)	-1.45

Ave Mechanical Collector Output

Oxygen %	9.1
CO(ppm)	0.10
Combustibles %	35
Temperature (F)	352
Static Press(in H2O)	-3.20

Utility Modernization Analysis

Boiler Calc. Sheet II

Coal Boilers

	Btu/lb	T amb (F)	Flue gas (F)
HHV	13500	345.0	80
Combustion Eff		86.57%	
Fuel	% lb/lb AF	lb/lbmol	lbmol/lb AF
C	70.41%	12	0.05868
H2	4.83%	2	0.02415
O2	8.28%	32	0.00259
N2	1.41%	28	0.00050
S	1.01%	32	0.00032
H2O (liq)	8.05%	18	0.00447
Ash	6.08%	MW	Mole Fract
Total	100.07%		

Flue Gas Losses

Dry Gas	Water Vapor	Unacctd.	Total Loss
0.07951	0.03977	0.01500	13.43%

Stoichiometric Excess Air

Balance C, H2 and S for stoichiometric conditions. Balance O2, N2 at excess air conditions.

Dry gas loss includes sensible heat in water vapor. Water vapor loss include fuel moisture and H2 formation. 1.5% unaccounted in coal.

Solution balances the combustion equation for stoichiometric conditions and then calculates excess air and recalculates flue gas products and properties

Air	
N2	79.00%
O2	21.00%
Incremental Excess Air	
Excess Air %	

0.32037002
0.25319359
0.06730463

0.04358
65%

Flue Gas % Gas Vol (dr Dry Gas Fract LbMoles/lb fuel

	% Gas Vol	dr Dry Gas Fract	LbMoles/lb fuel
O2	8.40%	8.40%	0.08400
CO (ppm)	30.00	0.00%	0.00003
CO2	not meas		0.05750
Combustibles	0.10%	0.10%	0.00100
NOx (ppm)		0.00%	0.00000
SOx (ppm)		0.00%	0.00000
H2O			0.02862
N2			0.25357
SO2			0.00032
			0.42504

Assume 2% carbon loss to ash (98% C forms CO2)

Gas	Polynomial Coeff	deg F	deg K	cp	cp ave (Btu/lb/lbmole/lb fuel	Btu/lb fuel deg F
	a	b	c			
CO2	10.34	0.00274	-195500	10.3767231	10.3767231	0.05750 0.59667714
SO2	7.7	0.0053	0.00000083	10.0680811	10.0680811	0.00032 0.00317774
H2O	8.22	0.00015	0.00000134	8.51845543	8.51845543	0.02862 0.24381712
N2	6.5	0.001		6.91927778	6.91927778	0.4174389 2.8883757
O2	8.27	0.000258	-187700	7.31044579	7.31044579	0.04358 0.31860699
					Sum	4.05065469

Polynomial equations from Perry's Chemical Handbook Table 3-181, Originally from US Bureau of Mines Bull 371, 1934 and USBM Bull 477, 1948.

Utility Modernization Analysis

Boiler Data Sheet

Boiler Test Data (Unit #3) - DSCC, Columbus, OH

Enerac ESP Outlet

26-Nov-96

Time	8:14:33	8:15:23	8:21:18	8:30:02	8:40	8:50
Combustion Eff(%)	96.9	97.6	98.1	97.6	97.2	97.1
Amb Temp (F)	51	51	50	49	47	46
Stack Temp (F)			259	258	259	261
O2 (dry)	10.5%	10.5%	10.6%	10.2%	10.6%	10.8%
CO(ppm)	24	20	20	29	26	26
CO2	7.8%	9.0%	8.9%	9.2%	8.9%	8.8%
Combustibles	0.00%	0.00%	0.00%	0.03%	0.05%	0.06%
StackDraft(neg"H2O)	1.3	1.5	1.5	1.8	1.9	1.8
Excess Air %	94%	96%	97%	91%	98.0%	101.0%
NOx (ppm)	142	187	193	206	222	245
SOx (ppm)	0	0	36	77	113	142

Time	9:00	9:10	9:20	9:30	9:40:06	
Combustion Eff(%)	96.7	96.7	96.5	96.3	96.4	
Amb Temp (F)	44	43	43	42	42	
Stack Temp (F)	263	263	267	265	266	
O2 (dry)	11.2%	10.8%	10.8%	11.1%	11.0%	
CO(ppm)	26	26	29	26	26	
CO2	8.4%	8.7%	8.7%	8.5%	8.6%	
Combustibles	0.07%	0.07%	0.08%	0.09%	0.09%	
StackDraft(neg"H2O)	1.9	2.3	2.3	2.3	2.8	
Excess Air %	109.0%	102.0%	102.0%	108.0%	105%	
NOx (ppm)	239	255	247	229	242	
SOx (ppm)	161	176	197	209	209	

Utility Modernization Analysis

Boiler Calc. Sheet I

Boiler Test Data

Fuel (Btu/lb) 13500

Ave. Enerac Data

26-Nov-96

(ESP Outlet)

Time	8:28
Combustion Eff(%)	97.4
Amb Temp (F)	49
Stack Temp (F)	259
O2 (dry)	10.5%
CO(ppm)	24
CO2	8.8%
Combust	0.02%
StackDraft(neg"H2O)	1.6
Excess Air %	96.2%
NOx (pm)	199
SOx (ppm)	92

Calculated

N2	80.70%
Excess Air	NA ??
Excess Air	NA ??

Fuel Curve

MBtu/gal	13500
Excess Air	
Eff (w/o rad)	
Rad Loss	
Eff (w/rad)	0.0%

Ave. Enerac Data

26-Nov-96

(ESP Outlet)

Time	9:20
Combustion Eff(%)	96.5
Amb Temp (F)	43
Stack Temp (F)	265
O2 (dry)	11.0%
CO(ppm)	27
CO2	8.6%
Combust	0.08%
StackDraft(neg"H2O)	2.3
Excess Air %	105.2%
NOx (pm)	242
SOx (ppm)	190

Utility Modernization Analysis

HTW Plant Data

Auxiliary Equipment (ESP #2)

Precipitator #2

25-Nov-96

Time	16:00	16:10	16:20	16:30	16:40	16:50
Primary Volts x 10	36	30	36	18	26	26
Primary Amps x 10	3.7	2.8	3.7	0.97	1.9	2.2
Secondary kV1	0	0	0	0	0	0
Secondary Amps	0.25	0.21	0.25	0.09	0.14	0.18
Secondary kV2	0	0	0	0	0	0
Sparks/Min x 10	0.0	0.0	0.2	0	0.6	0.8
Arcs/Min x 10		0.0	0	0	0.4	0

Time 17:00 17:10

Primary Volts x 10	16	30
Primary Amps x 10	0.79	2.7
Secondary kV1	0	0
Secondary Amps	0.07	0.24
Secondary kV2	0	0
Sparks/Min x 10	1.6	1.8
Arcs/Min x 10	0	1.4

Precipitator #2

26-Nov-96

Time	8:40	8:50	9:00	9:10	9:20	9:30
Primary Volts x 10				34	32	30
Primary Amps x 10				2.5	3.1	2.3
Secondary kV1				0	0	0
Secondary Amps				0.16	0.25	0.25
Secondary kV2				0	0	0
Sparks/Min x 10				0.6	0.6	0.6
Arcs/Min x 10				0.2	0	0.2

Utility Modernization Analysis

HTW Plant Data

Auxiliary Equipment (ESP #2) -- Average Values

Precipitator #2

25-Nov-96

Average

Time	16:35
Primary Volts x 10	27
Primary Amps x 10	2.35
Secondary kV1	0
Secondary Amps	0.18
Secondary kV2	0
Sparks/Min x 10	0.6
Arcs/Min x 10	0.3

Precipitator #2

26-Nov-96

Average

Time	9:20
Primary Volts x 10	32
Primary Amps x 10	2.6
Secondary kV	0
Secondary Amps	0.22
Secondary kV2	0
Sparks/Min x 10	0.6
Arcs/Min x 1	0.1

Utility Modernization Analysis

Boiler NDT Data Sheet

Boiler Test Data (Unit #3) - DSCC, Columbus, OH
Boiler Tube Testing

Rear Wall		Right Wall		Left Wall
top (straight)	elbow (bend)	top	bottom	top
0.103		0.113	0.112	0.106
	0.148	0.112	0.115	0.108
0.101		0.117	0.109	0.106
0.108		0.111	0.111	0.124
0.097		0.110	0.108	0.126
0.109		0.112	0.109	0.110
	0.146	0.112		0.110
0.108		0.111		0.108
0.106				
0.106				
0.109				

Minimum	0.097
Ave.	0.112

** Calibration factor = 0.253.

NOTES: 1. The rear wall tubes above are identified as follows -- left-to-right, the thicknesses are for every fifth tube, starting with the second tube from the left.

The right wall is the wall to the right when looking from the front to the rear of the generator. "Top" measurements were taken about 5-feet high for every tenth tube going from right to left and starting with the second tube from the right. "Bottom" measurements were taken about 2-feet high for every tenth tube starting with the tenth tube from the right, the top and bottom measurements thus being staggered.

Left wall measurements were taken about 5-feet high going from left to right, starting with the second tube from the left.

2. Comments regarding physical condition of HTW generator. Grate: T-Bar warped; edge seal leaks; chain wear right side sprockets; some skidshoe wear excessive. Convection pass: tubes OK. Air heater: four holes in duct wall, Upper W and N, Lower N and E. MDC: exit OK; top tubes worn; spinners worn; C2 spinner backwards; lower C3 broken almost all around; boot tab broken D2, A6, B7 and E7.

Boiler NDT Calc Sheet

Boiler Tube Testing

Tube Type	SA 178 grA
Stress Factor (ASME Code)	11800
Temp (F)	600
Tube OD (in)	2.25
e factor	0

Utility Modernization Analysis

Boiler NDT Data Sheet

Boiler Test Data (Unit #1) - DSCC, Columbus, OH

Boiler Tube Testing

Rear Wall (Top)	Rear Wall (Elbow)	Right Wall	Left Wall
--------------------	----------------------	------------	-----------

0.111	0.127	0.111	0.106
0.102	0.118	0.107	0.107
0.092	0.12	0.101	0.107
0.102		0.108	0.106
0.103		0.104	0.108
0.108		0.109	0.106
0.111		0.106	0.105
0.134			
0.139			

Minimum	0.092
Ave.	0.110

Comments regarding physical condition of HTW generator. Grate: T-Bar bowed; endclip seals not working; OK to fire this Winter; rear-top air seal - overgrate seal shoes crystallized; rear right TC gone; some skid shoes worn down; left end - one rail bent, clip binding. Backpass: failed refractory; tubes need air lancing; header plugs leaking; backwall tubes pushed out. MDC: lots of flyash in East hopper; bottom lower tubes worn severely; Row A spinners clogged; dampers for upper MDC not working; upper tubes severely worn; hole in E3 tube; spinners severely worn; exit has mud; rope packing needed in x-joint.

Boiler Test Data (Unit #1) - DSCC, Columbus, OH

Data taken 11/26/96 for HTW Generator #1, down due to leaking tubes

Furnace Roof, R-L Tube #	12" from knuckle	At knuckle	Calibra- tion Factor	Missing Tubes
2	0.103	0.128	0.26	10
4	0.18		0.26	30
6 (hole)	0.107		0.26	34
8	0.107		0.26	35
23	0.15		0.25	
25	0.119		0.25	
27	0.13		0.25	
29	0.132		0.25	
31	0.144		0.25	
32	0.152		0.25	
33	0.152		0.25	

Minimum	0.103
Ave.	0.134

Boiler NDT Calc Sheet

Tube Type	SA 178 grA
Stress Factor (ASME Code)	11800
Temp (F)	600
Tube OD (in)	2.25
e factor	0

Utility Modernization Analysis

MDC Inspection

Unit #1

Top Tubes

	E	D	C	B	A
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					

Dirty Gas In



Top Tube Tube Sheet (clean gas outlet)

	E	D	C	B	A
1					
2					
3					
4					
5					
6					
7					
8					
9					Clogged
10					Clogged

Dirty Gas In



Bottom Tube (Ash hopper inspection)

	E	D	C	B	A
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					

Dirty Gas In



Other Notes:

Utility Modernization Analysis

MDC Inspection

Unit #3

Top Tubes

	E	D	C	B	A
1					
2	Worn		Spin Bkwd		
3	Worn				
4	Worn				
5	Worn				
6	Worn				
7	Worn				
8	Worn				
9					
10					

Dirty Gas In →

Top Tube Tube Sheet (clean gas outlet)

	E	D	C	B	A
1					
2					
3					
4					
5					
6					
7					
8					
9					
10					

Dirty Gas In →

Bottom Tube (Ash hopper inspection)

	E	D	C	B	A
1					
2					
3			Broken		
4					
5					
6					
7					
8					
9					
10					

Dirty Gas In →

Other Notes:

Pipe Schedule Thickness Correction

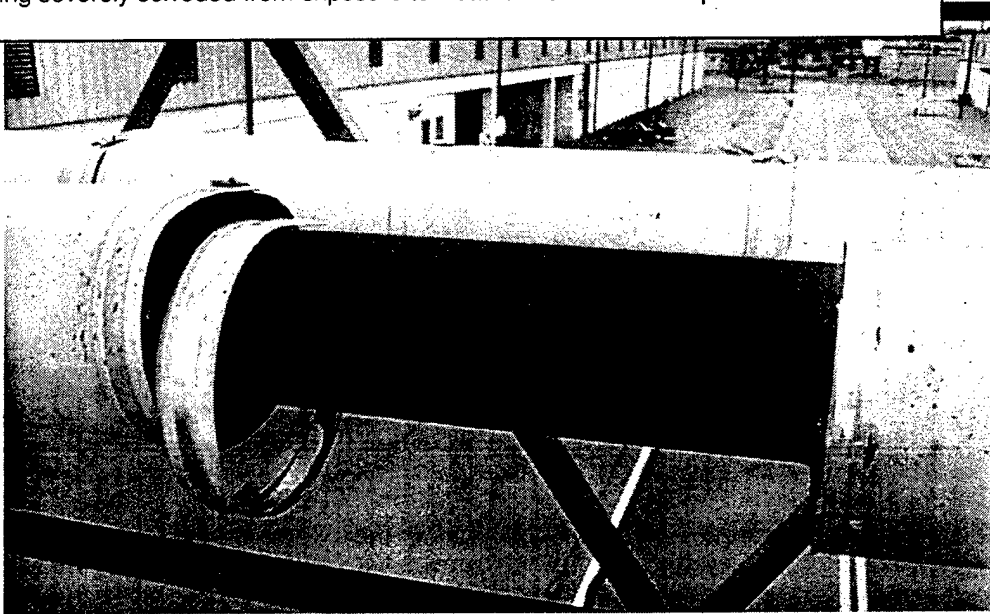
Size	Temperature 400		Std Temp 70	
	Sched 40	Sched 80	Sched 40	Sched 80
3	0.216	0.300	0.212	0.295
4	0.237	0.337	0.233	0.331
5	0.258	0.375	0.254	0.369
6	0.280	0.432	0.275	0.425
8	0.322	0.500	0.317	0.492
10	0.365	0.593	0.359	0.583
12	0.406	0.687	0.399	0.676
14	0.438	0.750	0.431	0.738
16	0.500	0.843	0.492	0.829

Thickness Testing

Site Bldg 17-18 Crossover Cold Wall (in)
 Pipe Size 6 0.280
 Pipe Temp 400 Std Temp 70
 Air Temp 35

Location	Thickness	Corrected	Notes
Top 12	0.311	0.306	
1:30	0.302	0.297	
Side 3	0.287	0.282	
4:30	0.307	0.302	
Bottom 6	0.306	0.301	
		0.000	
Top 12	0.317	0.312	
1:30	0.315	0.310	
Side 3	0.309	0.304	

Piping severely corroded from exposure to weather. Schedule 40 specified.

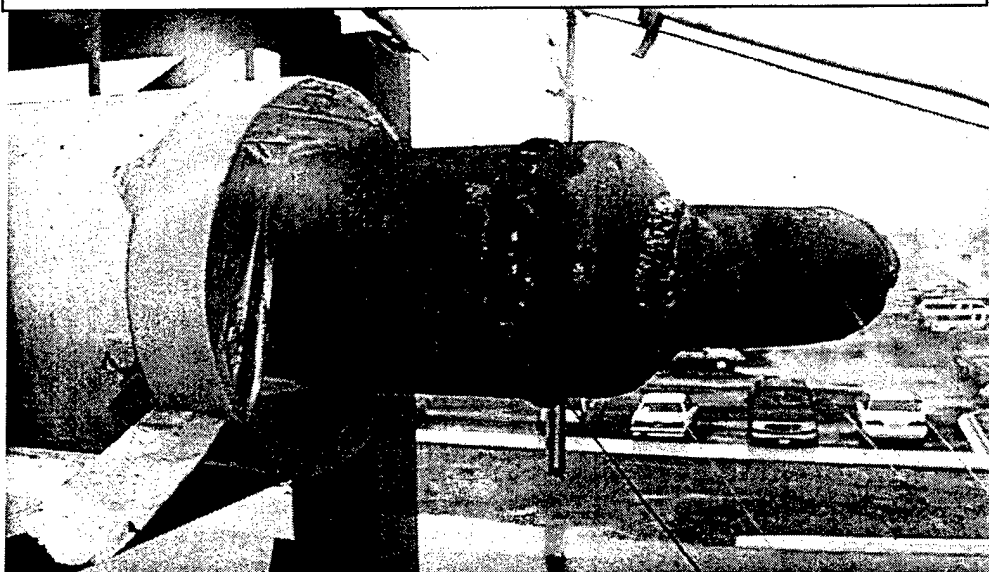


Thickness Testing

Site	Bldg 12, S end		Cold Wall (in)
Pipe Size	6		0.280
Pipe Temp	420	Std Temp	70
Air Temp	34		

Location	Thickness	Corrected	Notes
Top 12	0.330	0.324	
1:30	0.301	0.296	
Side 3	0.313	0.308	
4:30	0.288	0.283	
Bottom 6	0.235	0.231	
7:30	0.281	0.276	
Side 9	0.273	0.268	
10:30	0.301	0.296	
		0.000	

Piping only moderately corroded from exposure to weather. Schedule 40 specified.

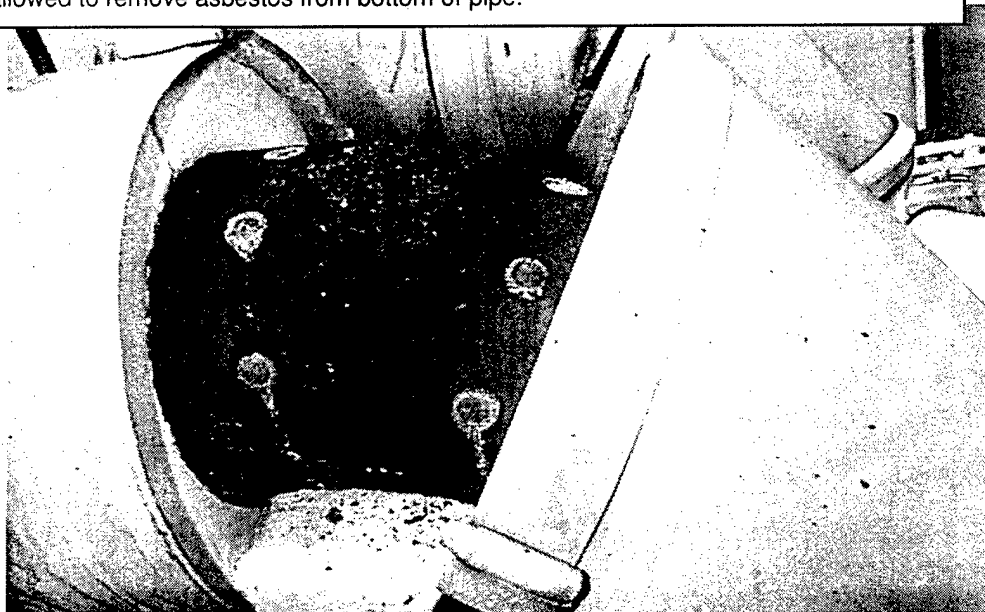


Thickness Testing

Site Bldg 30 S side Cold Wall (in)
Pipe Size 6 0.280
Pipe Temp 407 Std Temp 70
Air Temp 34

Location	Thickness	Corrected	Notes
Top 12	0.278	0.273	
1:30	0.284	0.279	
Side 3	0.303	0.298	
		0.000	
Top 12	0.280	0.275	
1:30	0.252	0.248	
Side 3	0.300	0.295	
		0.000	
		0.000	

Piping only moderately corroded from exposure to weather. Schedule 40 specified. Not allowed to remove asbestos from bottom of pipe.

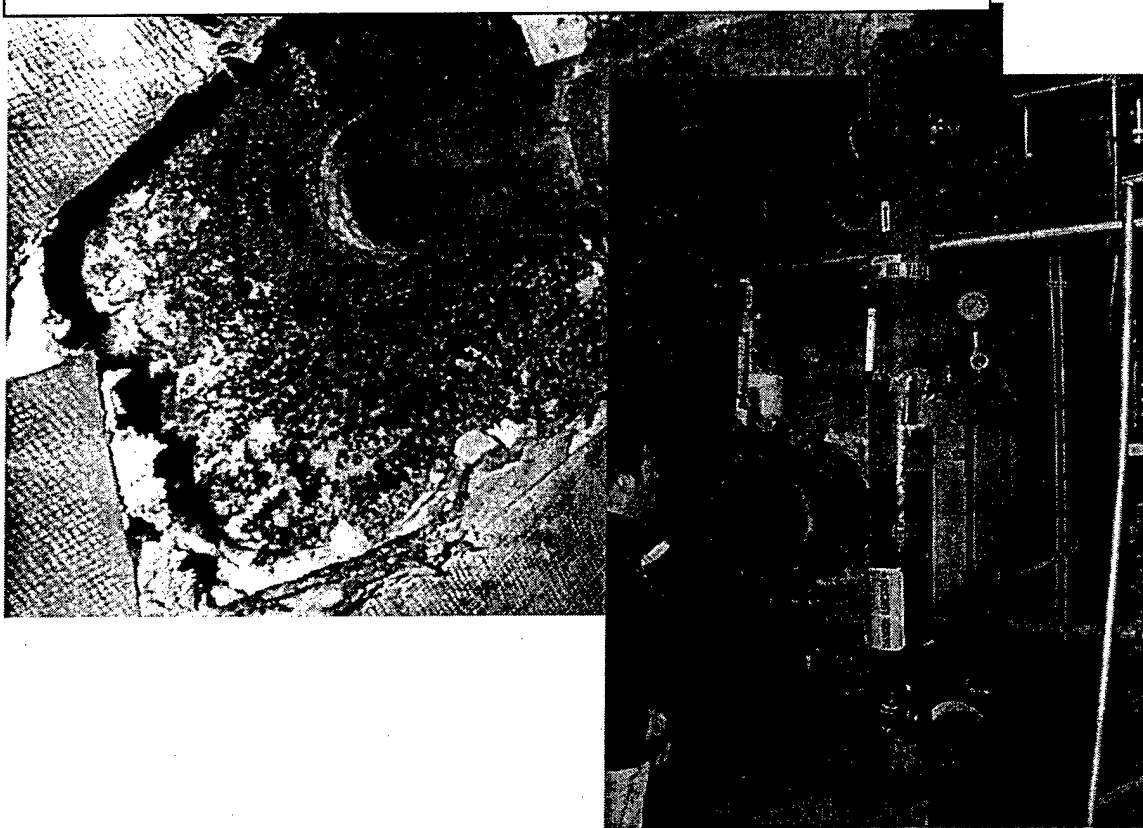


Thickness Testing

Site	Bldg 30 Mech room Converter		Cold Wall (in)
Pipe Size	Unk		Unk
Pipe Temp	237	Std Temp	70
Air Temp	86		

Location	Thickness	Corrected	Notes
Bottom	0.451	0.447	
		0.000	

Vessel corroded. Nameplate not readable. Recommend checking waterline thickness.

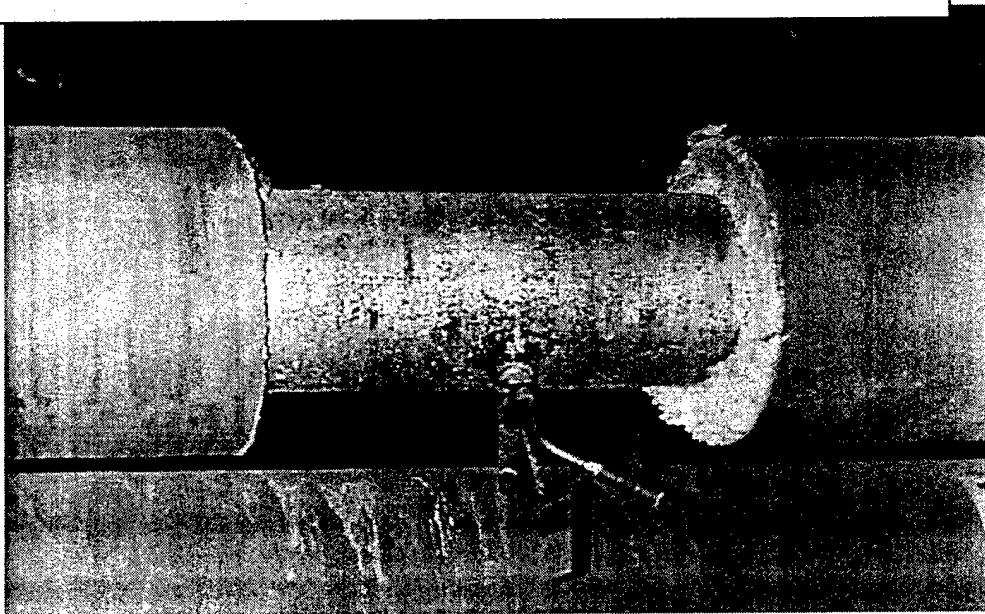


Thickness Testing

Site Bldg 30 Mech Room Cold Wall (in)
Pipe Size 6 0.280
Pipe Temp 375 Std Temp 70
Air Temp 86

Location	Thickness	Corrected	Notes
Top 12	0.281	0.277	
1:30	0.272	0.268	
Side 3	0.280	0.276	
4:30	0.270	0.266	
Bottom 6	0.299	0.294	
		0.000	
		0.000	
		0.000	
		0.000	

Piping not corroded as not exposed to weather. Schedule 40 specified.



Appendix B: Nalco Metallurgical Analysis



DSCC
COLUMBUS, OHIO

Nalco Metallographic Analysis No. 076564

Specimen: Hot Water Boiler

Sampling Date: January 16, 1997

CONTENTS

A. Nalco Metallographic Analysis Report

B. Photographs

1. As-received Boiler Tube Sections
2. Photograph of a Split Section Showing the Internal Surface Deposit and/or Corrosion Product Layer Present on One Side of the Tube
3. Close-up of the Smooth Internal Surface Contour
4. Close-up of a Depression Underlying the Deposit and/or Corrosion Product Layer Shown in Figure 2
5. Microstructure Consisting of Partially Spheroidized Pearlite in a Ferrite Matrix
6. Micrograph Showing a Region of Nearly Complete Decarburization
7. Micrograph Showing a Shallow, Oxide-filled Depression on the Internal Surface
8. Micrograph Showing a Fairly Thick External Surface Oxide Layer

NALCO CHEMICAL COMPANY
ONE NALCO CENTER • NAPERVILLE, ILLINOIS 60563-1188



NALCO METALLOGRAPHIC ANALYSIS

Analysis No. 076564

FROM: DSCC
COLUMBUS, OHIO

DESCRIPTION OF SAMPLE

Three sections of boiler tubing were received for metallurgical analysis, Figure 1. The sections were reportedly removed from a 300 psi hot water boiler. The sections have lengths of 20", 19", and 14-3/4". The outer diameter of each section is 1-1/4". The sections were submitted following failures in the top wall section of the boiler. No failure is present on any of the received sections.

The internal surface of each section contains a deposit and/or corrosion product layer on one side of the tube, Figure 2. A sample of the material overlying the surface was scraped and submitted for x-ray analysis. The results of this analysis will be forwarded upon completion. The surface contour is mostly smooth, Figure 3. The side of the section which contains the deposit and/or corrosion product exhibits scattered, mostly shallow depressions. The deepest measured depression reduced the wall thickness by 0.020", Figure 4.

The external surface is covered by a thin brown deposit which overlies a thick layer of thermally deteriorated metal (iron oxide). The surface contour appears mostly smooth.

MICROSCOPIC EXAMINATIONS

Seven specimens were cut from the sections at selected locations and prepared for microscopic examination. The microstructure in some locations examined consists of partially spheroidized pearlite in a ferrite matrix, Figure 5. Other locations, however, exhibited almost complete decarburization, Figure 6.

A series of nine microhardness measurements were conducted on the mounted specimens. The average Knoop hardness number was 108.

The internal surface profile is mostly smooth. Specimens removed from the side of the tube containing the deposit and/or corrosion product exhibited scattered, shallow, oxide-filled depressions, Figure 7. A moderately thick, dense iron oxide layer is present in places.

The external surface profile is smoothly undulating. A thick iron oxide layer is present in places, Figure 8. The maximum measured



NALCO METALLOGRAPHIC ANALYSIS

Analysis No. 076564

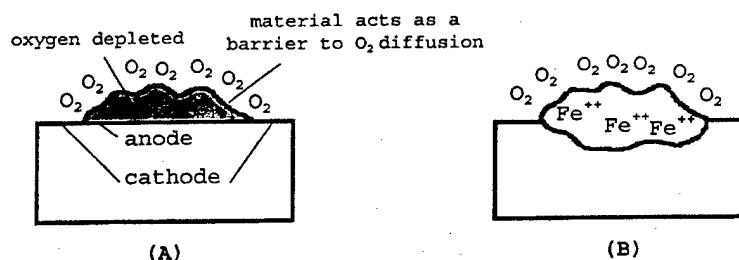
FROM: DSCC
COLUMBUS, OHIO

thickness of the oxide is 0.014", as measured using an optical microscope equipped with a calibrated video imaging system.

CONCLUSION

The received sections contain no failure. The internal surface of one side of each section contains a deposit and/or corrosion product layer. Scattered depressions are present on this side of the tube. Most of the metal loss is shallow, however, the deepest measured depression reduced the wall thickness by 0.020". The appearance of the attack most closely resembles oxygen corrosion.

Oxygen corrosion resulted from exposure of metal surfaces to waters containing dissolved oxygen. The resulting corrosion product shields the underlying metal and acts as a barrier to oxygen diffusion. As a result, a local area of reduced oxygen concentration develops [see (A) below]. A difference in electrochemical potential exists between regions of a metal in contact with waters containing different levels of dissolved oxygen. This difference in potential results in corrosion (B).



The presence of oxygen attack on only one side of each section indicates that the damage most likely occurred during an idle period or periods.

Specific interest was expressed in the composition of the material overlying the internal surface. A sample was scraped from the surface and submitted for analysis. Results of the analysis will be forwarded upon completion.



NALCO METALLOGRAPHIC ANALYSIS

Analysis No. 076564

FROM: DSCC
COLUMBUS, OHIO

Analysis indicated that the section experienced long term, mild overheating. Microstructural evidence indicated that metal temperatures between 850 and 1050°F were reached for an extended period. The reported overheating occurred due to excessive heat input relative to coolant flow rate. Three possible causes of excessive heat input relative to coolant flow rate are:

1. Excessive heat input with specified coolant flow.
2. Specified heat input with insufficient coolant flow.
3. Excessive heat input with insufficient coolant flow.

As a result of overheating, a significant amount of oxidation has occurred. The maximum measured external surface oxide thickness was 0.014". No bulging or other significant damage resulted from the overheat.

A. C. BIONDO

Words and concepts referred to in this report are discussed and illustrated in *The Nalco Guide to Boiler Failure Analysis*.

ACB:dmc
3/7/97



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Analysis No. 076564

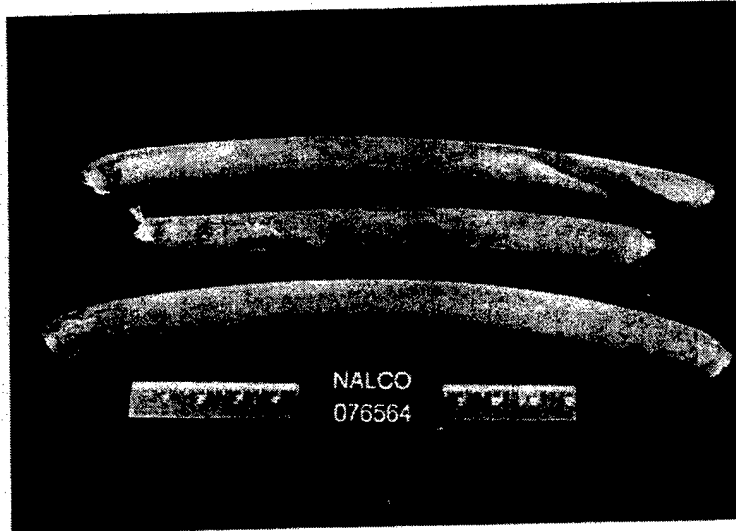


Figure 1
As-received Boiler Tube Sections

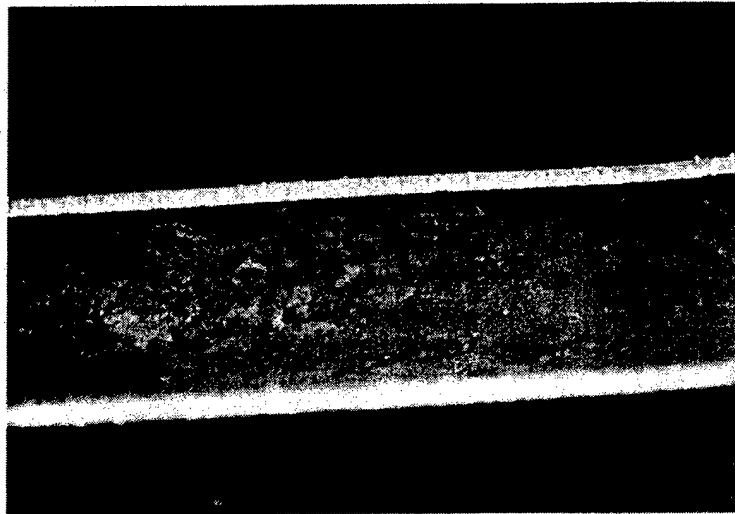


Figure 2
Photograph of a Split Section Showing the Internal Surface Deposit
and/or Corrosion Product Layer Present on One Side of the Tube

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Analysis No. 076564

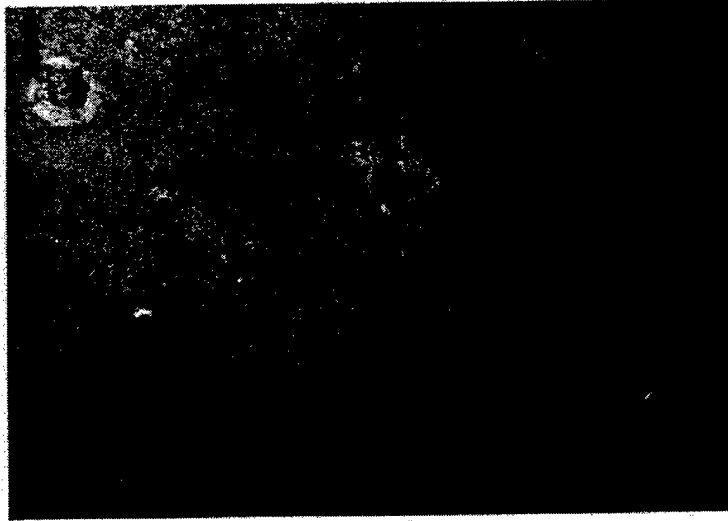


Figure 3
Close-up of the Smooth Internal Surface Contour

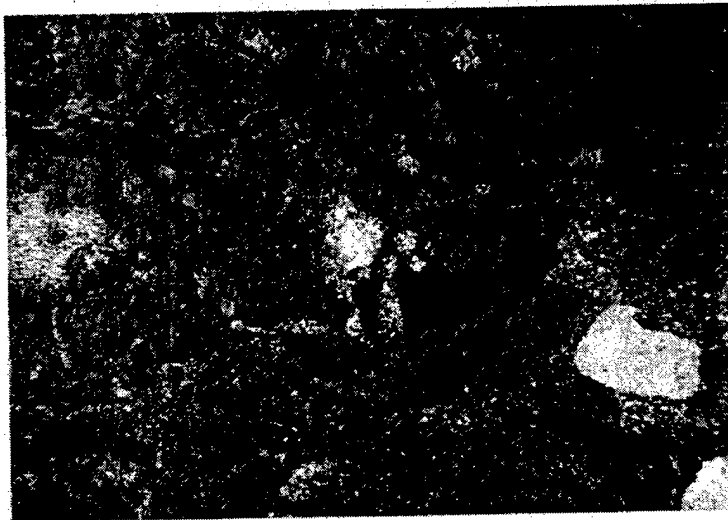


Figure 4
Close-up of a Depression Underlying the
Deposit and/or Corrosion Product Layer Shown in Figure 2

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Analysis No. 076564

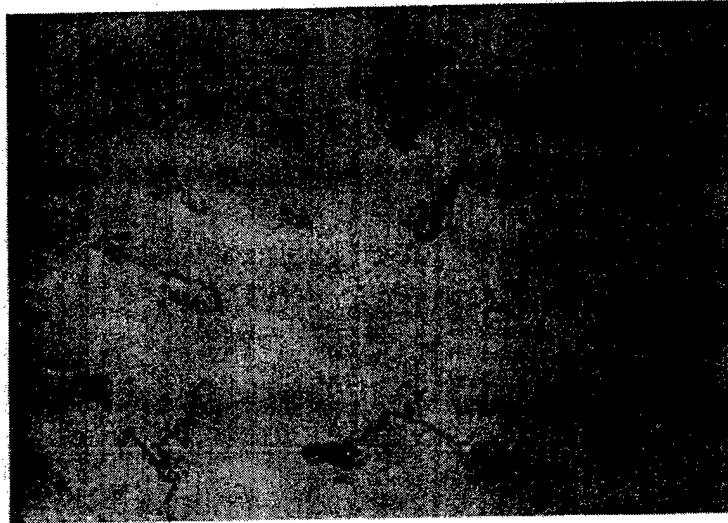


Figure 5
Microstructure Consisting of Partially
Spheroidized Pearlite in a Ferrite Matrix
Magnification: 1000x Etchant: Picral

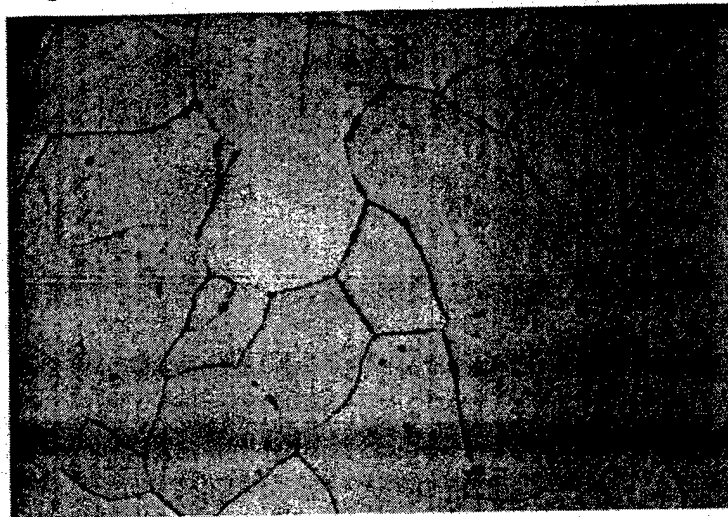


Figure 6
Micrograph Showing a Region of
Nearly Complete Decarburization
Magnification: 1000x Etchant: Nital



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Analysis No. 076564



Figure 7
Micrograph Showing a Shallow, Oxide-filled
Depression on the Internal Surface
Magnification: 500x Etchant: Nital



Figure 8
Micrograph Showing a Fairly Thick External Surface Oxide Layer
Magnification: 200x Etchant: Picral

Appendix C: HEATMAP Data Output

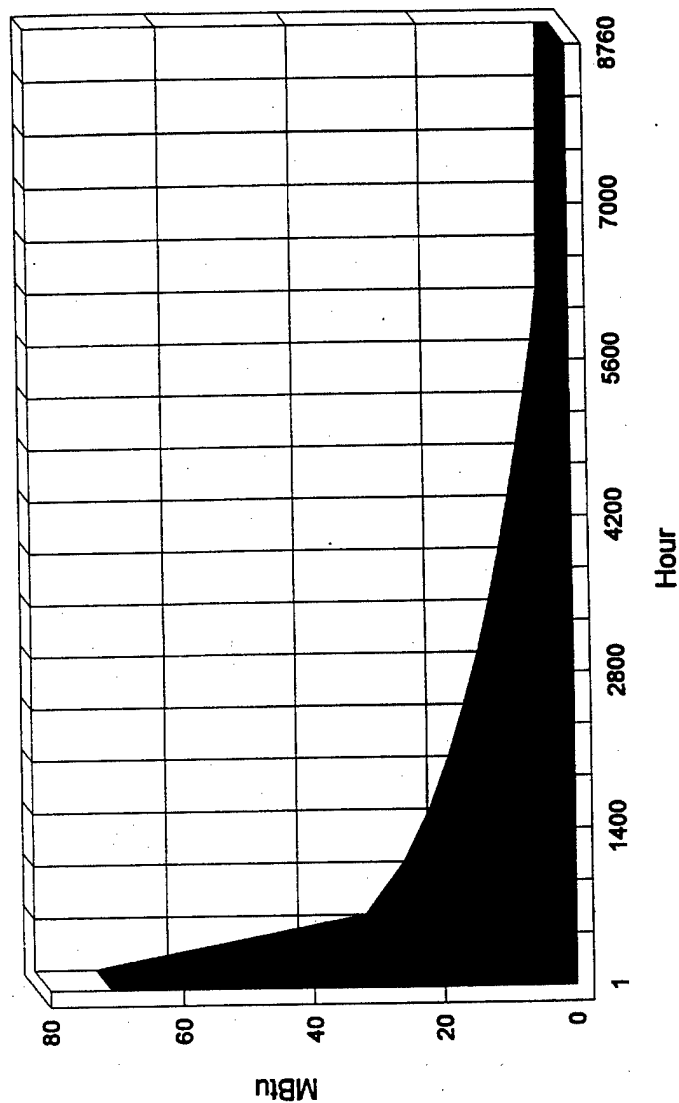
July 6, 1998

Page 1

HEATMAP Consumer Load Summary 101 - New Scenario

ID	Consumer name	(Sq Ft)	Heating Annual (MBtu/yr)	Heating Peak (kBtu/hr)	Hot water Annual (MBtu/yr)	Hot water Peak (kBtu/hr)	Process Annual (MBtu/yr)	Process Peak (kBtu/hr)	Total Annual (MBtu/yr)	Total Peak (kBtu/hr)
40	Consumer 40	28,070	504.8	658.3	106.5	24.3	0.0	0.0	611.3	682.6
100	Demolish	2,802	45.5	125.5	13.3	3.0	0.0	0.0	58.8	128.5
10-2	after indiv. heating	21,730	390.8	530.8	82.5	18.8	0.0	0.0	473.3	549.6
1	Demolish	270,500	4,865.0	5,037.2	1,026.4	234.3	0.0	0.0	5,891.4	5,271.5
41	Plus 42, Stay heated wet/dry	735,798	12,980.6	15,520.0	3,491.9	797.2	0.0	0.0	16,472.5	16,317.2
27	Stay wet/heated OR dry/cold	283,183	4,986.0	6,249.2	1,344.0	306.8	0.0	0.0	6,340.0	6,556.0
30	wet to dry and cold	174,307	3,134.9	3,344.2	661.4	151.0	0.0	0.0	3,796.3	3,495.2
150	Demolition scheduled	26,381	379.1	740.1	125.2	28.6	0.0	0.0	504.3	768.7
2	Demolition Scheduled	247,800	4,458.5	4,641.7	940.7	214.8	0.0	0.0	5,399.2	4,856.5
5	Demolish	246,400	3,918.6	4,544.4	935.0	213.5	0.0	0.0	4,853.6	4,757.9
306	Demolish	56,218	991.8	1,420.1	266.8	60.9	0.0	0.0	1,256.6	1,481.0
308	Install indiv. heating	51,230	736.1	1,325.0	243.1	55.5	0.0	0.0	978.2	1,380.5
17	Wet to dry and cold	176,948	3,182.4	3,391.1	671.4	153.3	0.0	0.0	3,853.8	3,544.4
18	Wet to dry and cold	174,383	3,138.3	3,345.6	661.7	151.1	0.0	0.0	3,798.0	3,496.7
49	Plus 46	1,720	30.3	90.2	8.2	1.9	0.0	0.0	38.5	92.1
10	Wet to dry S 1-6 and cold, S	130,638	2,349.5	2,564.3	495.7	113.2	0.0	0.0	2,845.2	2,671.5
19	Wet to dry and cold	174,383	3,136.3	3,345.6	661.7	151.1	0.0	0.0	3,798.0	3,496.7
9	Install indiv. heating	283,213	5,093.6	5,259.2	1,074.7	245.4	0.0	0.0	6,168.3	5,504.6
11b	Staying wet and heated	86,265	1,551.5	1,759.0	327.3	74.7	0.0	0.0	1,878.8	1,833.7
12b	Staying dry and heated	131,200	2,314.7	3,053.2	622.7	142.2	0.0	0.0	2,937.4	3,195.4
12a	Staying dry and heated	152,000	2,681.6	3,068.6	721.4	164.7	0.0	0.0	3,403.0	3,661.3
11a	Staying wet and heated	196,935	3,474.4	4,445.5	934.6	213.4	0.0	0.0	4,408.0	4,659.9
TOTAL:		3,652,200	64,352.3	74,887.8	15,416.2	3,519.7	0.0	0.0	79,768.4	76,407.5

Load Duration Curve --- 87,507 (MBtu/Yr)

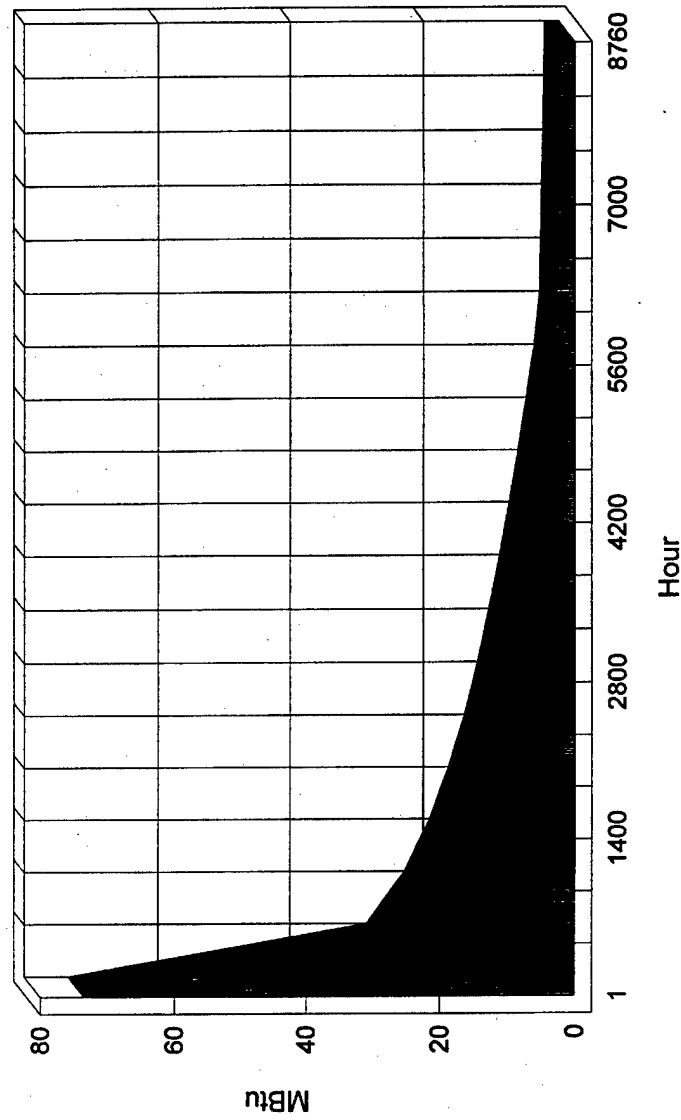


July 6, 1998

HEATMAP Scenario: New Scenario

HEATMAP Consumer Load Summary 103 - LTW										Page 1
ID	Consumer name	(Sq Ft)	Heating Annual (MBtu/Yr)	Heating Peak (kBtu/Hr)	Hot water Annual (MBtu/Yr)	Hot water Peak (kBtu/Hr)	Process Annual (MBtu/Yr)	Process Peak (kBtu/Hr)	Total Annual (MBtu/Yr)	Total Peak (kBtu/Hr)
10-2	after indiv. heating	21,730	390.8	530.8	82.5	18.8	0.0	0.0	473.3	549.6
100	Demolish	2,802	45.5	125.5	13.3	3.0	0.0	0.0	58.8	128.5
1	Demolish	270,500	4,865.0	5,037.2	1,026.4	234.3	0.0	0.0	5,891.4	5,271.5
40	Consumer 40	28,070	504.8	658.3	106.5	24.3	0.0	0.0	611.3	682.6
41	Plus 42, Stay heated wet/dry	735,786	12,980.6	15,520.0	3,491.9	797.2	0.0	0.0	16,472.5	16,317.2
27	Stay wet/heated OR dry/cold	283,183	4,986.0	6,249.2	1,344.0	306.8	0.0	0.0	6,340.0	6,556.0
30	wet to dry and cold	174,307	3,134.9	3,344.2	661.4	151.0	0.0	0.0	3,796.3	3,495.2
150	Demolition scheduled	26,381	379.1	740.1	125.2	28.6	0.0	0.0	504.3	768.7
2	Demolition Scheduled	247,900	4,458.5	4,841.7	940.7	214.8	0.0	0.0	5,398.2	4,855.5
5	Demolish	246,400	3,918.6	4,544.4	835.0	213.5	0.0	0.0	4,853.6	4,757.9
306	Demolish	56,218	981.8	1,420.1	268.8	60.9	0.0	0.0	1,256.6	1,481.0
308	Install indiv. heating	51,230	736.1	1,325.0	243.1	55.5	0.0	0.0	979.2	1,380.5
17	Wet to dry and cold	176,948	3,182.4	3,391.1	671.4	153.3	0.0	0.0	3,853.8	3,544.4
18	Wet to dry and cold	174,383	3,136.3	3,345.6	681.7	151.1	0.0	0.0	3,788.0	3,488.7
49	Plus 46	1,720	30.3	90.2	8.2	1.9	0.0	0.0	38.5	92.1
10	Wet to dry S 1-6 and cold, S	130,636	2,349.5	2,564.3	495.7	113.2	0.0	0.0	2,845.2	2,677.5
19	Wet to dry and cold	174,383	3,136.3	3,345.6	681.7	151.1	0.0	0.0	3,788.0	3,488.7
9	Install indiv. heating	283,213	5,093.6	5,259.2	1,074.7	245.4	0.0	0.0	6,168.3	5,504.6
11b	Staying wet and heated	86,285	1,551.5	1,759.0	327.3	74.7	0.0	0.0	1,878.8	1,833.7
12b	Staying dry and heated	131,200	2,314.7	3,053.2	622.7	142.2	0.0	0.0	2,937.4	3,195.4
12a	Staying dry and heated	152,000	2,581.6	3,496.6	721.4	164.7	0.0	0.0	3,403.0	3,661.3
11a	Staying wet and heated	196,935	3,474.4	4,446.5	934.6	213.4	0.0	0.0	4,409.0	4,659.9
TOTAL:		3,652,200	64,352.3	74,887.8	15,416.2	3,519.7	0.0	0.0	79,768.4	76,407.5

Load Duration Curve --- 87,090 (MBtu/Yr)



HEATMAP Scenario: LTW

April 9, 1999

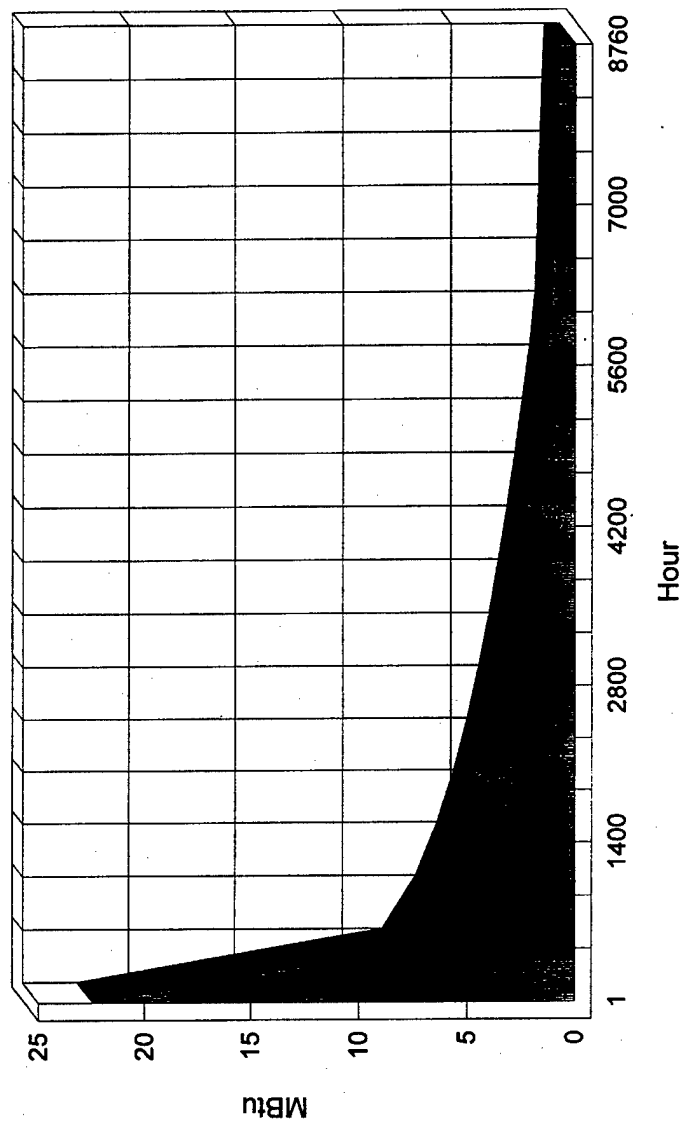
July 6, 1998

Page 1

HEATMAP Consumer Load Summary 105 - HTW with dry pipe/demolition

ID	Consumer name	(Sq Ft)	Heating Annual (MBtu/Yr)	Heating Peak (kBtu/Hr)	Hot water Annual (MBtu/Yr)	Hot water Peak (kBtu/Hr)	Process Annual (MBtu/Yr)	Process Peak (kBtu/Hr)	Total Annual (MBtu/Yr)	Total Peak (kBtu/Hr)
40	Consumer 40	28,070	504.8	658.3	106.5	24.3	0.0	0.0	611.3	682.6
9a	after indiv. heating	43,626	784.6	961.6	165.5	37.8	0.0	0.0	950.1	999.4
10-2	after indiv. heating	21,730	380.8	530.8	82.5	18.8	0.0	0.0	473.3	549.6
41	Plus 42, Stay heated wet/dry	735,796	12,980.6	15,520.0	3,491.9	797.2	0.0	0.0	16,472.5	16,317.2
27	Stay wet/heated OR dry/cold	283,183	4,996.0	6,249.2	1,344.0	306.8	0.0	0.0	6,340.0	6,556.0
308	Install indiv. heating	51,230	736.1	1,325.0	243.1	55.5	0.0	0.0	979.2	1,380.5
11b	Staying wet and heated	86,265	1,551.5	1,759.0	327.3	74.7	0.0	0.0	1,878.8	1,833.7
12b	Staying dry and heated	131,200	2,314.7	3,053.2	622.7	142.2	0.0	0.0	2,937.4	3,195.4
12a	Staying dry and heated	152,000	2,681.6	3,496.6	721.4	164.7	0.0	0.0	3,403.0	3,661.3
11a	Staying wet and heated	196,935	3,474.4	4,446.5	934.6	213.4	0.0	0.0	4,409.0	4,659.9
TOTAL:		1,730,035	30,415.1	38,000.2	8,039.5	1,835.4	0.0	0.0	38,454.6	39,835.6

Load Duration Curve ---- 26,763 (MBtu/Yr)



HEATMAP Scenario: HTW (demo, dry pipe, 41&42 ind heat)

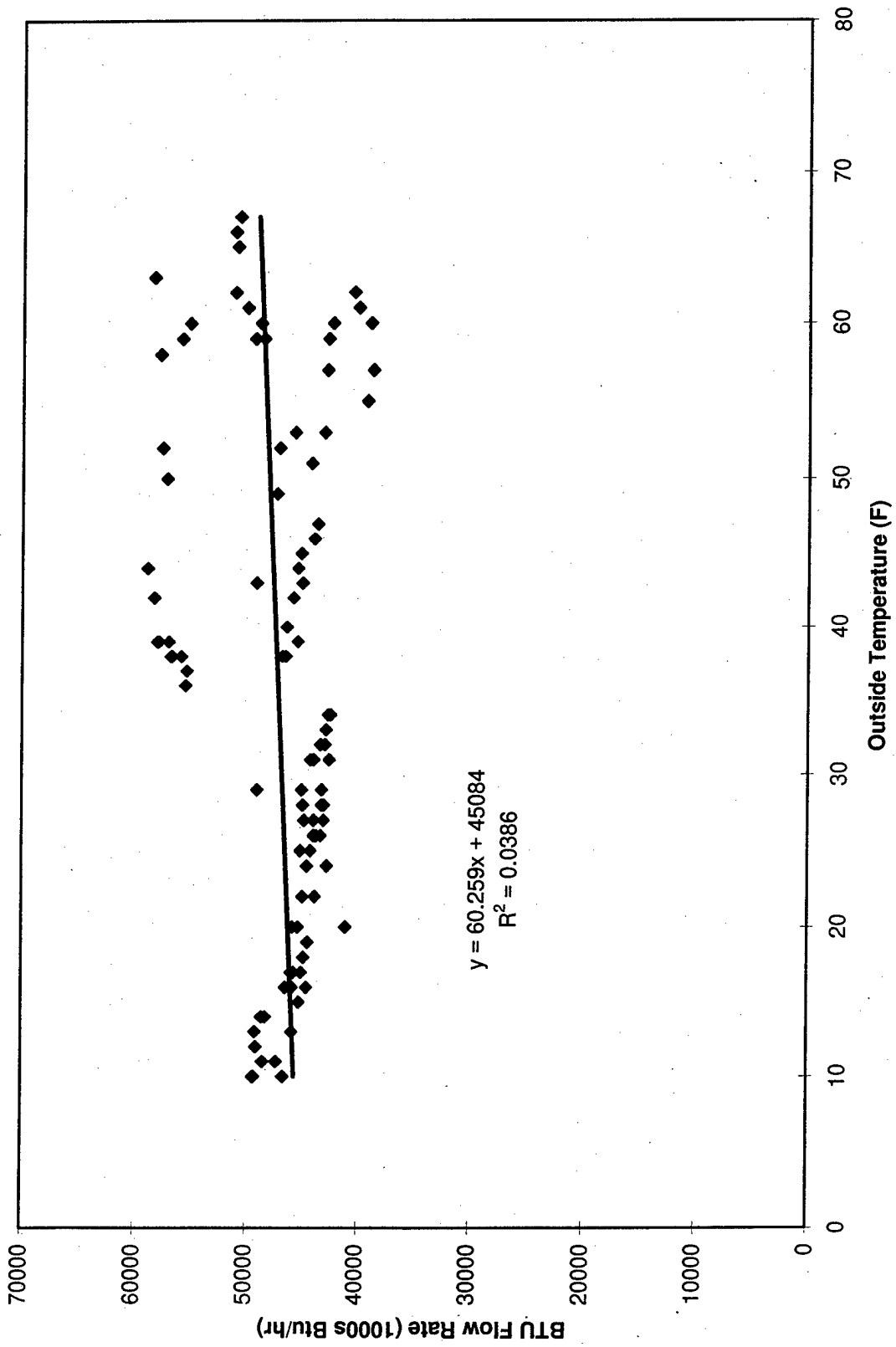
April 9, 1999

Appendix D: CHP Modernization Analysis Data Sheets

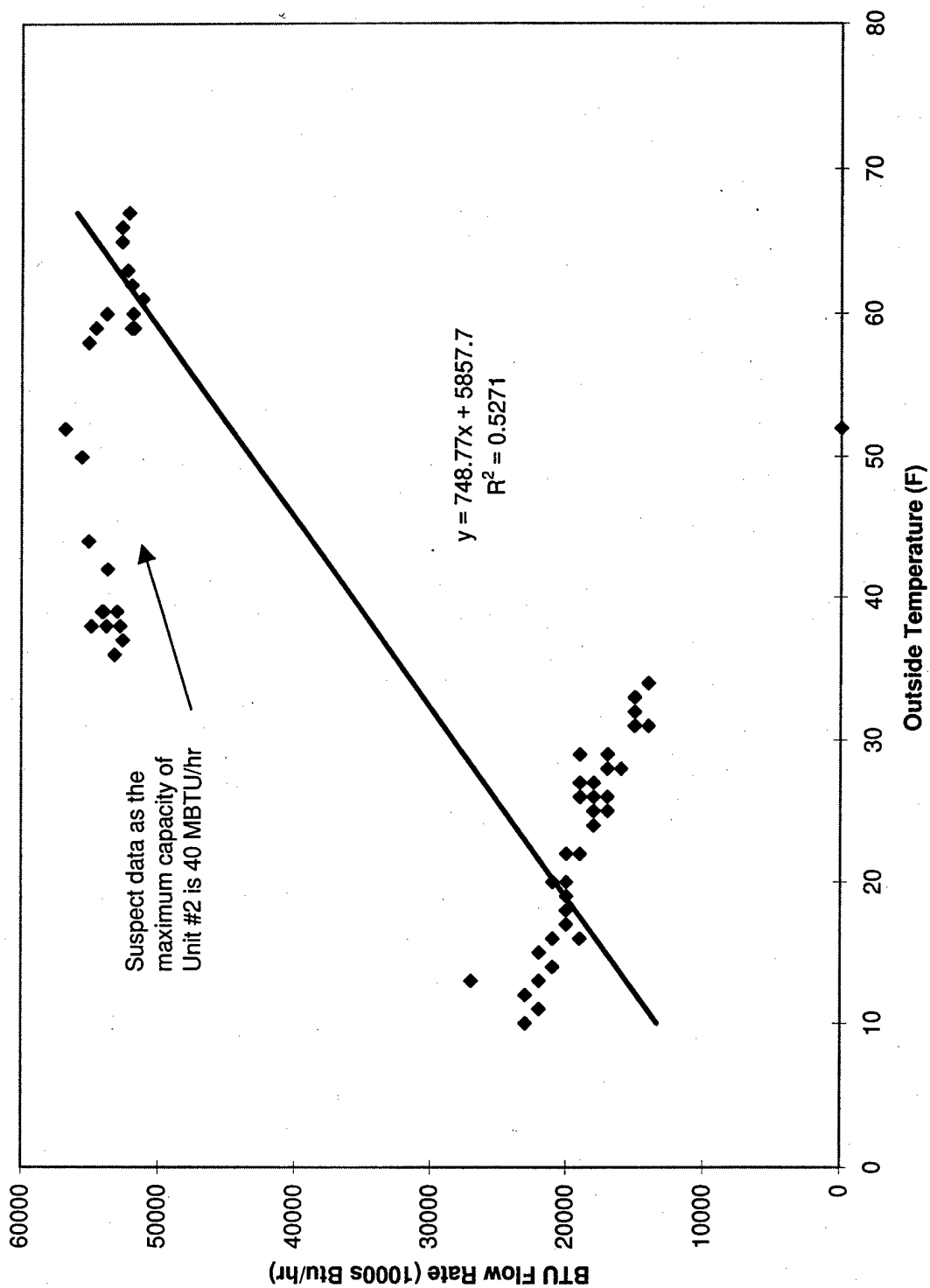
Utility Modernization Analysis						Option List		
Option	Production Peak Load MBTU/hr	Bldg Served Sq. ft.	Coal Fuel MBTU/yr	Gas Fuel MBTU/yr	Oil Fuel MBTU/yr	Elect MWhr/yr	Bldg Peak Loan MBTU/hr	
Base Case	1	80.8	3,652,200	106,669		514	78.4	
	2	80.8	3,652,200	106,669		514	78.4	
	2a	80.8	3,652,200	106,669		514	78.4	
	3	80.8	3,652,200		102,904	427	78.4	
	3a	80.8	3,652,200		102,904	427	78.4	
	3a-1	80.8	3,652,200		102,904	427	78.4	
	3b	41.2	1,730,035		50,166	292	39.8	
	3c	41.2	1,730,035		50,166	292	39.8	
	3c-1	41.2	1,730,035		50,166	292	39.8	
	4	80.8	3,652,200		102,904	427	78.4	
	5	80.8	3,652,200	96,001.92	10,290	427	78.4	
	6	80.8	3,652,200			102,904	427	78.4
	6a	80.8	3,652,200			102,904	427	78.4
	7	80.8	3,652,200			102,904	427	78.4
	7a	41.2	3,652,200			102,904	427	78.4
	8	78.4	3,652,200		93,845		427	78.4
	8a	39.9	1,730,035		45,241		292	39.9
	9	78.4	3,652,200		93,845		427	78.4
	9a	39.9	1,730,035		45,241		292	39.9
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Appendix E: LCCID Output

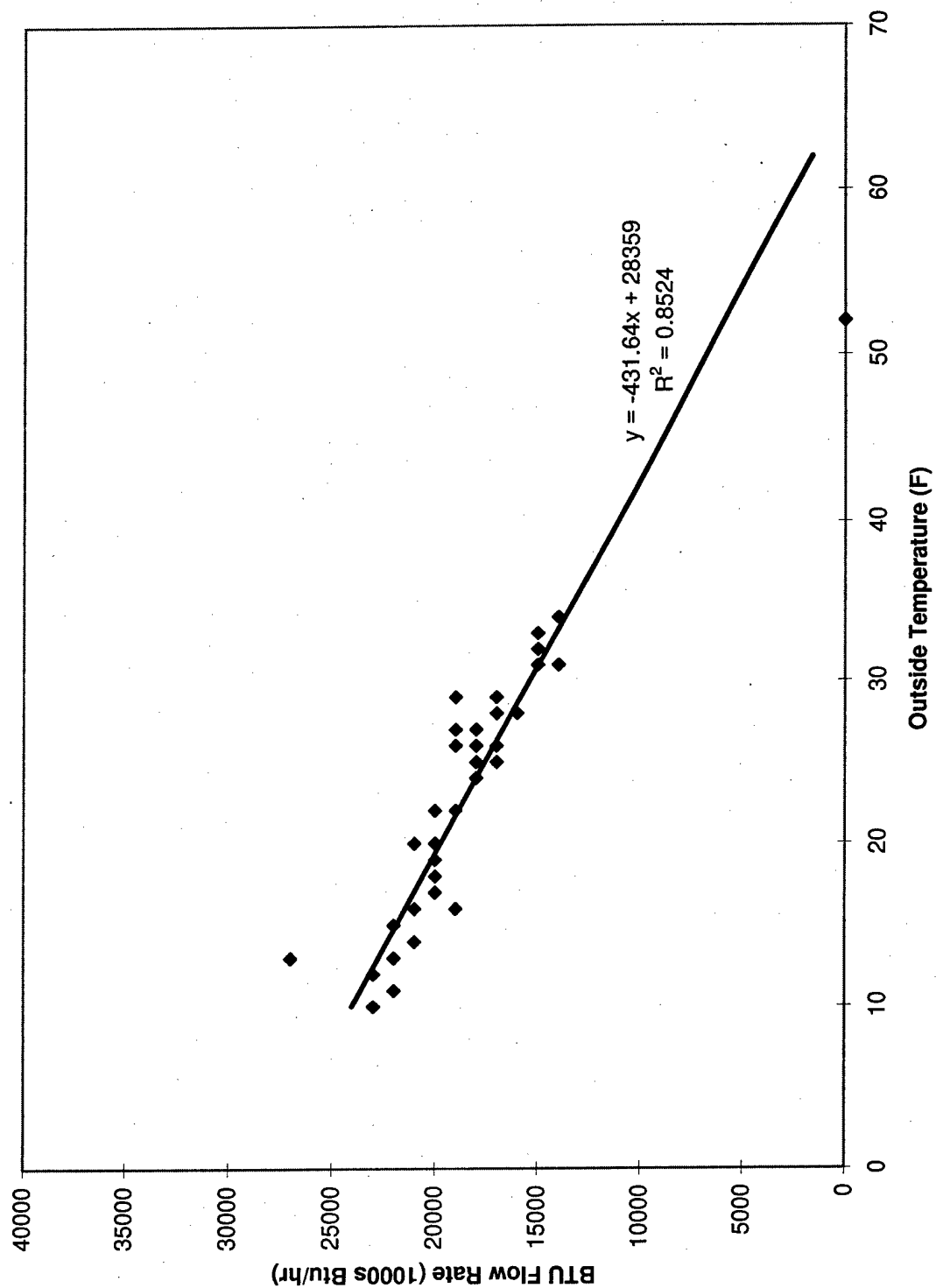
HTHW Unit 1 BTU Flow Rate vs. Outside Temperature



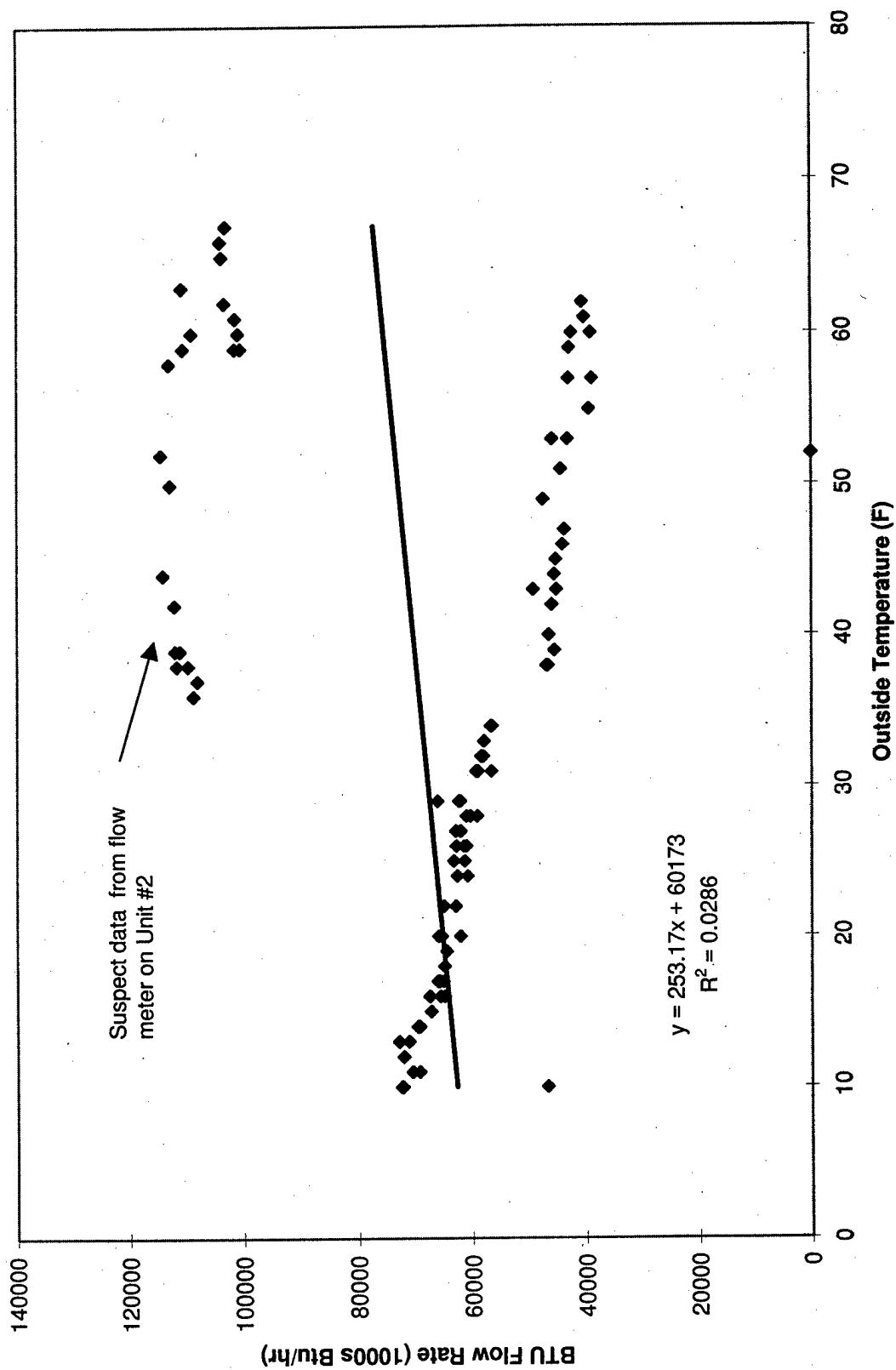
HTHW Unit # 2 BTU Flow Rate vs. Outside Temperature



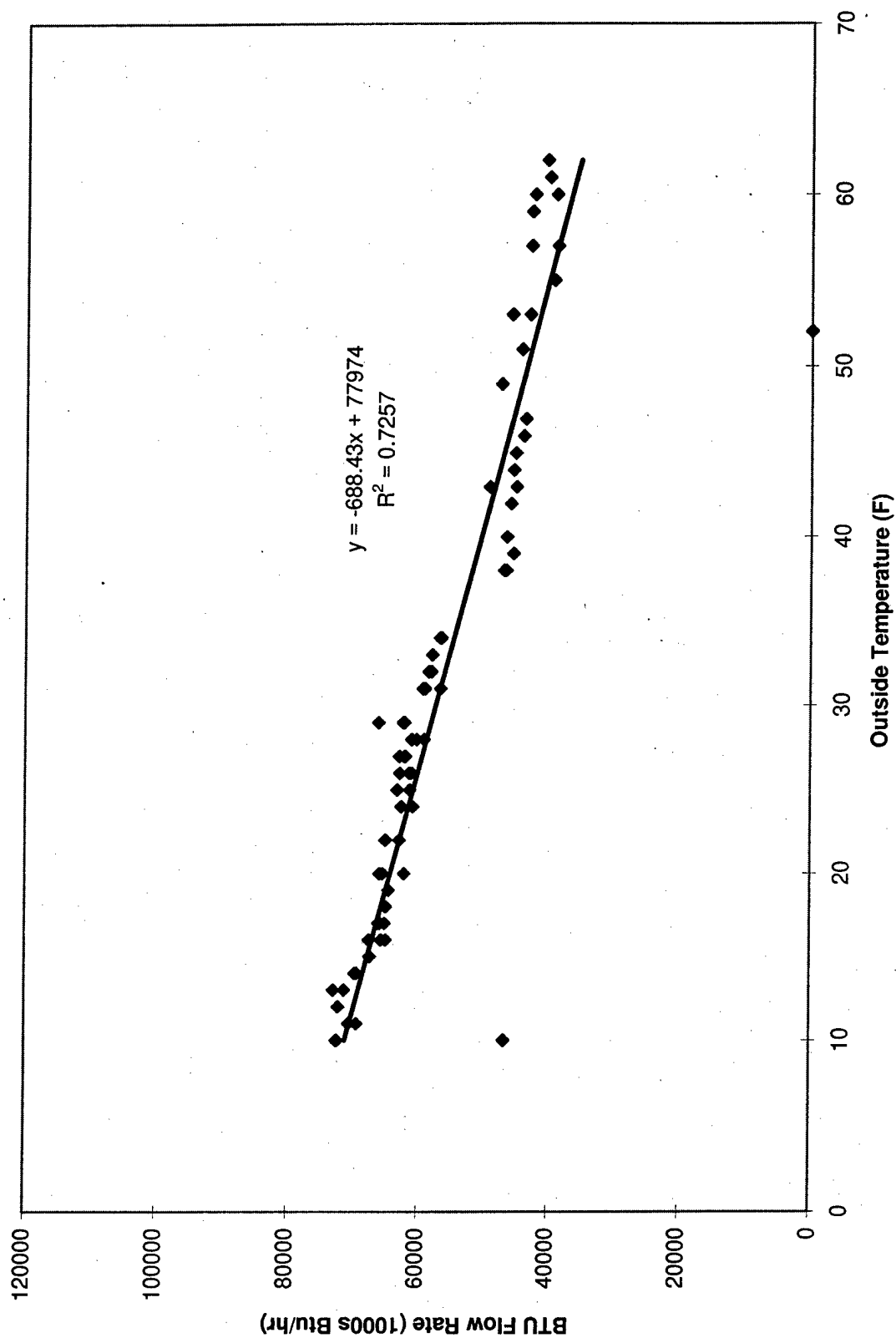
HTHW Unit #2 BTU Flow Rate vs. Outside Temperature



Total BTU Flow Rate vs. Outside Temperature

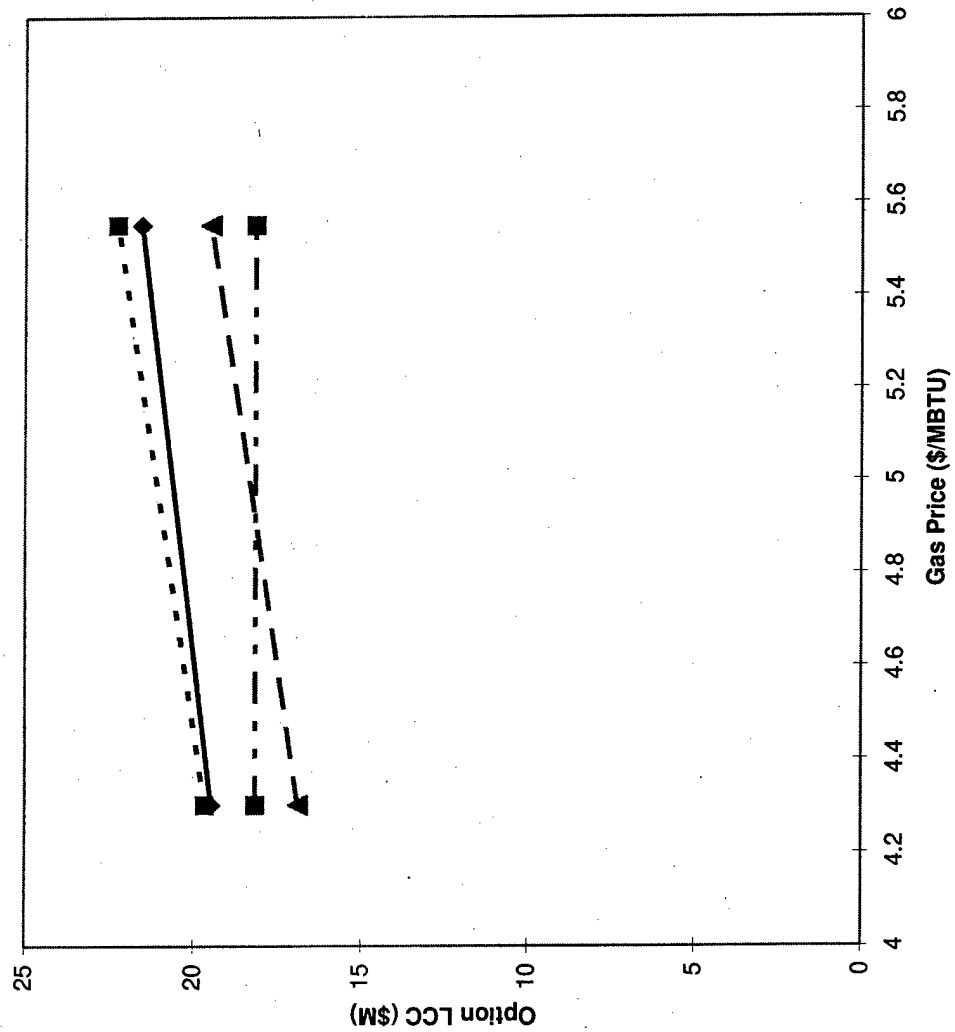


Total BTU Flow Rate vs. Outside Temperature

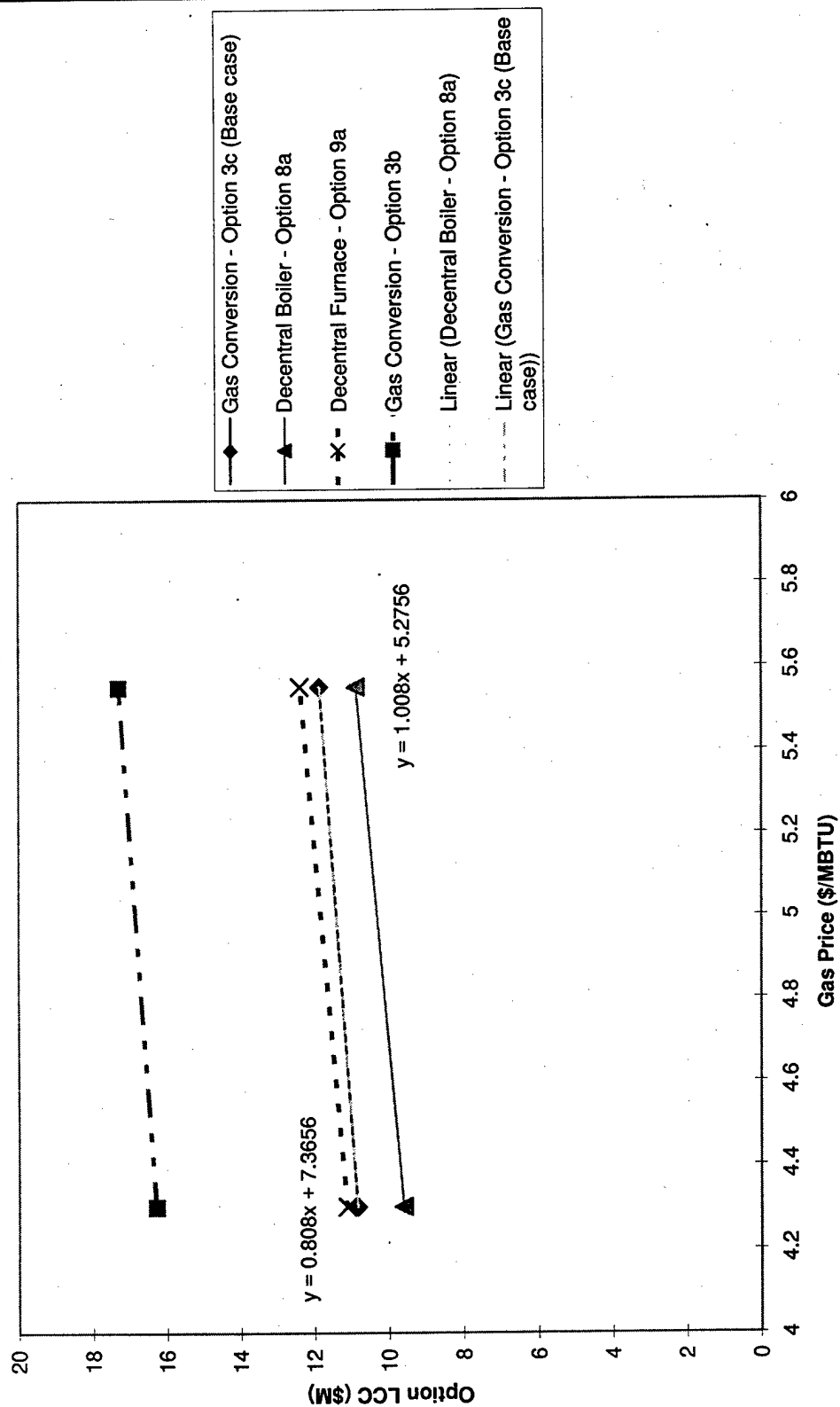


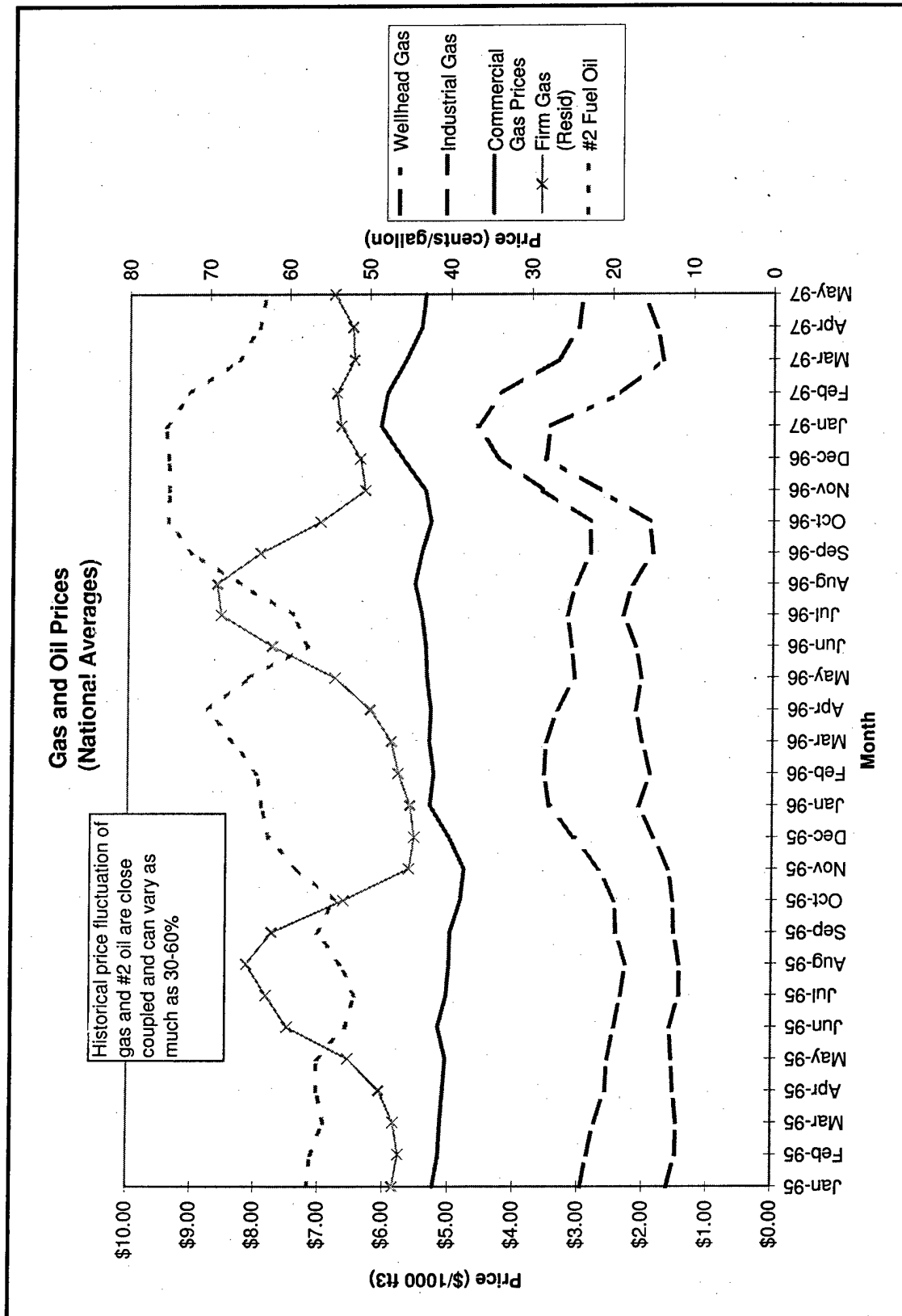
Appendix F: Net Present Value Sensitivity Analysis

Effect of 29% Increase in Fuel Price on LCC Analysis



Effect of 29% Increase in Fuel Price on LCC Analysis





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